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(57) Abstract: Disclosed are plastic preforms and bottles, preferably comprising polyethylene terephthalate (PET), in which the materials in the neck, neck finish and/or neck cylinder is at least partially in the crystalline state and the body is primarily in the amorphous or semi-crystalline state. This structure in a preform enables the preform to be easily blow molded by virtue of the amorphous material in the body, while being able to have dimensional stability in hot-fill applications. In addition, the amorphous inner surface of the neck finish stabilizes the post mold dimensions allowing closer molding tolerances than other crystallizing processes. On the other side, the crystallized outer surface supports the amorphous structure during high temperature filling of the container. Physical properties are also enhanced as a result of this unique crystalline/amorphous structure.

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**BOTTLES AND PREFORMS HAVING A CRYSTALLINE NECK**Background of the InventionField of the Invention

This invention relates to plastic bottles and containers such as for containing beverages and the like. More specifically, this invention relates to plastic bottles, preferably comprising polyethylene terephthalate (PET), in which the materials in the neck, neck finish and/or neck cylinder is at least partially in the crystalline state. Such bottles and preforms also preferably comprise one or more layers comprising RPET, a material which acts as a barrier to oxygen and carbon dioxide, or an oxygen scavenger.

Description of the Related Art

10 The use of plastic containers as a replacement for glass or metal containers in the packaging of beverages has become increasingly popular. The advantages of plastic packaging include lighter weight, decreased breakage as compared to glass, and potentially lower costs. The most common plastic used in making beverage containers today is PET. Virgin PET has been approved by the FDA for use in contact with foodstuffs. Containers made of PET are transparent, thin-walled, lightweight, and have the ability to maintain their shape by withstanding the force exerted on  
15 the walls of the container by pressurized contents, such as carbonated beverages. PET resins are also fairly inexpensive and easy to process.

Most PET bottles are made by a process which includes the blow-molding of plastic preforms which have been made by processes including injection molding. In some circumstances, it is preferred that the PET material in plastic preforms is in an amorphous or semi-crystalline state because materials in this state can be readily blow-  
20 molded where fully crystalline materials generally cannot. However, bottles made entirely of amorphous or semi-crystalline PET may not have enough dimensional stability during a standard hot-fill process due to the relatively low  $T_g$  of the PET material and the tight tolerances required when using standard threaded closures. In these circumstances, a bottle comprising crystalline PET would be preferred, as it would hold its shape during hot-fill processes.

Summary of the Invention

25 In preferred embodiments, the present invention provides for a plastic bottle, which has the advantages of both a crystalline PET bottle and a amorphous or semi-crystalline PET bottle. By making at least part of the uppermost portion of the preform crystalline while keeping the body of the preform amorphous or semi-crystalline (sometimes referred to herein as "non-crystalline"), one can make a preform that will blow-mold easily yet retain  
30 necessary dimensions in the crucial neck area during a hot-fill process. The preform and bottle may be made solely of PET or another crystalline material, preferably a polyester, or it may further comprise other materials, including barrier materials and/or oxygen scavenger materials to prevent carbonated beverages or oxygen-sensitive products contained within the bottle from going "flat" or spoiling.

Such processes preferably accomplish the making of a preform within the preferred cycle times for uncoated  
35 PET preforms of similar size by standard methods currently used in preform production. Further, the preferred

processes are enabled by tooling design and process techniques to allow for the simultaneous production of crystalline and amorphous regions in particular locations on the same preform.

In accordance with a preferred embodiment, an article is provided which comprises a neck portion and a body portion. The neck portion and the body portion are a monolithic first layer of material. The body portion is primarily amorphous or semi-crystalline, and the neck portion is primarily crystalline.

In accordance with a preferred embodiment, there is provided a mold for making a preform comprising a neck portion having a first mold temperature control system, a body portion having a second temperature control system, and a core having a third temperature control system, wherein the first temperature control system is independent of the second and third temperature control systems and the neck portion is thermally isolated from the body portion and core.

#### Brief Description of the Drawings

FIGURE 1 is an uncoated preform as is used as a starting material for preferred embodiments of the present invention.

FIGURE 2 is a cross-section of a preferred uncoated preform of the type that is barrier-coated in accordance with one preferred embodiment.

FIGURE 3 is a cross-section of one preferred embodiment of barrier-coated preform.

FIGURE 4 is a cross-section of another preferred embodiment of a barrier-coated preform.

FIGURE 5 is a cross-section of a preferred preform in the cavity of a blow-molding apparatus of a type that may be used to make a preferred barrier-coated container.

FIGURE 6 is one preferred embodiment of barrier-coated container.

FIGURE 7 is a cross-section of an injection mold of a type that may be used to make a preferred barrier-coated preform.

FIGURES 8 and 9 are two halves of a molding machine to make barrier-coated preforms.

FIGURES 10 and 11 are two halves of a molding machine to make forty-eight two-layer preforms.

FIGURE 12 is a perspective view of a schematic of a mold with mandrels partially located within the molding cavities.

FIGURE 13 is a perspective view of a mold with mandrels fully withdrawn from the molding cavities, prior to rotation.

FIGURE 14 is a three-layer embodiment of a preform.

FIGURE 15 is a cross-section of an injection mold of a type that may be used to make a preferred preform of the present invention;

FIGURE 16 is a cross-section of the mold of Figure 15 taken along lines 16-16;

FIGURE 17 is a cutaway close up view of the area of Figure 15 defined by line 17;

FIGURE 18 is a cross-section of an injection mold core having a double wall neck finish portion;

FIGURE 19 is a cross-section of an enhanced injection mold core having a high heat transfer base end portion.

Detailed Description of the Preferred Embodiment

The preferred embodiments described herein generally produce preforms with a crystalline neck, which are typically then blow-molded into beverage containers. The preforms may be monolayer; that is, comprised of a single layer of a base material, or they may be multilayer, including, but not limited to, those which comprise a combination of a base material and a barrier material and a combination of a base material and RPET. The material in such layers may be a single material or it may be a blend of one or more materials so as to include blends of polymers and/or inclusion of an oxygen scavenging material. The provision of one or more barrier layers, or the inclusion of an oxygen scavenger in one or more layers, is generally desirable when the container is to be filled with a carbonated beverage or oxygen sensitive product. The barrier layer serves to prevent the ingress of oxygen into the container or the egress of carbon dioxide from the container. Additionally, multiple barrier layers may be provided to refine barrier properties or provide desirable structural properties. For the sake of convenience, the barrier layer will be referred to in the singular, but is intended to include multiple barrier layers where appropriate and desired.

By achieving a crystallized state in the neck portion of the preform during the molding step, the final dimensions are substantially identical to the initial dimensions, unlike when additional heating steps are used. Therefore, dimensional variations are minimized and dimensional stability is achieved. This results in more consistent performance of the threads on the neck finish and reduces the scrape rate of the molding process.

The preferred embodiments generally have a monolithic, or unitary, first layer which has both crystalline and amorphous or semi-crystalline regions. This results in a preform which has sufficient strength to be used in widespread commercial applications. A preform which has a both crystalline and amorphous or semi-crystalline regions is shown in U.S. Patent Number 6,217,818 to Collete et al. However, the preform of Collete et al. is constructed from a separately formed, crystalline neck portion. The neck portion is then placed into a second cavity which forms an amorphous body portion of the preform. However, this method has numerous drawbacks. For example, the arrangement of the pre-molded neck portion within the second, body forming, mold prevents venting of gases during the injection phase of the molding process. This would result in a void at the mechanical connection point between the neck and body portions and, thus, an insufficient connection. Additionally, the connection point between the neck and body portions is the last area of the mold cavity to receive injected material. As a result, there is poor flow of the melt at the point of the mold which forms the connection between the neck and body which would result in an insufficient mechanical connection between the two parts. Furthermore, the temperature of the injected material, or melt, is substantially low by the time it reaches the connection point, having travelled the full distance of the mold, that melt bonding would be minimal if it existed at all. Consequently, the method provided by Collette et al. is very unlikely to result in a commercially feasible preform, or container formed therefrom. Providing a monolithic first layer successfully overcomes the problems discussed above.

At least one of the preferred embodiments is provided with a barrier layer as described above. As such, the description may often refer to a barrier coated preform or finished bottle. References to barrier coated preform, however, should not give the impression that the present invention is confined only to multilayer preforms and

containers which comprise a base layer of PET and a second layer or barrier coating; monolayer preforms comprised of homopolymers or copolymers of PET or other such crystalline polymers and polyesters, multilayer preforms having more than two layers, preforms having at least one layer comprising RPET, and other such permutations including the materials noted above may also be made to have the crystallized thread and/or neck components described herein.

5 Furthermore, the embodiments described herein specifically describe use of polyethylene terephthalate (PET) but many other thermoplastics, including those of the polyester type may also be used. Examples of such other materials include polyethylene naphthalate (PEN), PETG, polytetramethylene 1,2-dioxybenzoate, copolymers of ethylene terephthalate and ethylene isophthalate, and Polyamide Blends, and recycled materials, such as RPET.

10 In especially preferred embodiments, "high IPA PET" is used as the polyester which is barrier coated. As it is used herein, the term "high-IPA PET" refers to PET to which IPA was added during to manufacture to form a copolymer in which the IPA content is more than about 2% by weight, preferably 2-10% IPA by weight, more preferably 3-8%, most preferably about 4-5% IPA by weight. The most preferred range is based upon current FDA regulations, which do not allow for PET materials having an IPA content of more than 5% to be in contact with food or drink. If such regulations are not a concern, then an IPA content of 5-10% is preferred. As used herein, "PET"

15 includes "high IPA PET."

The high-IPA PET (more than about 2% by weight) is preferred because the inventor has surprisingly discovered that use of high-IPA PET in the processes for making barrier preforms and containers, provides for better interlayer adhesion than is found in those laminates comprising PET with no IPA or low IPA. Additionally, it has been found that interlayer adhesion improves as the IPA content rises. Incorporation of the higher amounts of IPA into the

20 PET results in a decrease in the rate of crystallization of the high IPA PET material as compared to PET homopolymer, or PET having lower amounts of IPA. The decrease in the rate of crystallization allows for the production of PET layers (made of high IPA PET) having a lower level of crystallinity than what is achieved with low-IPA PET or homopolymer PET when they are made into barrier preforms by similar procedures. The lower crystallinity of the high-IPA PET is important in reducing crystallinity at the surface of the PET, i.e. the interface between the PET and the

25 barrier material. Lower crystallinity allows for better adhesion between the layers and also provides for a more transparent container following blow molding of the preform.

While a non-crystalline preform is preferred for blow-molding, a bottle having greater crystalline character is preferred for its dimensional stability during a hot-fill process. Accordingly, a preform constructed according to preferred embodiments has a generally non-crystalline body portion and a generally crystalline neck portion. To create

30 generally crystalline and generally non-crystalline portions in the same preform, one needs to achieve different levels of heating and/or cooling in the mold in the regions from which crystalline portions will be formed as compared to those in which generally non-crystalline portions will be formed. The different levels of heating and/or cooling are preferably maintained by thermal isolation of the regions having different temperatures. This thermal isolation between the thread split, core and/or cavity interface can be accomplished utilizing a combination of low and high thermal conduct

35 materials as inserts or separate components at the mating surfaces of these portions.

The cooling of the mold in regions which form preform surfaces for which it is preferred that the material be generally amorphous or semi-crystalline, is accomplished by chilled fluid circulating through the mold cavity and core. In preferred embodiments, a mold set-up similar to conventional injection molding applications is used, except that there is an independent fluid circuit or electric heating system for the portions of the mold from which crystalline portions of the preform will be formed.

Preferably, the preforms and containers have the barrier coating disposed on their outer surfaces or within the wall of the container. In contrast with the technique of Slat, which produces multilayered preforms in which the layers are readily separated, in preferred embodiments disclosed herein the thermoplastic barrier material adheres directly and strongly to the PET surface and is not easily separated therefrom. Adhesion between the layers results without the use of any additional materials such as an adhesive material or a tie layer. The coated preforms are processed, preferably by stretch blow molding to form bottles using methods and conditions similar to those used for uncoated PET preforms. The containers which result are strong, resistant to creep, shrinkage and are cosmetically appealing as well as having good gas-barrier properties.

One or more layers of a barrier material are employed in carrying out the methods of and making the articles according to preferred embodiments. As used herein, the terms "barrier material", "barrier resin" and the like refer to materials which, when used to form articles, preferably have key physical properties similar to PET, adhere well to PET, and have a lower permeability to oxygen and carbon dioxide than PET.

Once a suitable barrier material is chosen, an apparatus and method for economically manufacturing a container using the barrier material is necessary. One important method and apparatus involves using an injection molding machine in conjunction with a mold comprising a mandrel or core and a cavity. A first layer of a preform is molded between the mandrel and a first cavity of the mold when a molten polyester is injected therein. The first layer remains on the mandrel when the mandrel is pulled out of the cavity, moved, and inserted into a second mold cavity. A second layer of the material, preferably a barrier layer or a layer comprising barrier material, is then injected over the existing first preform layer. The mandrel and accompanying preform are then removed from the second cavity and a robot removes the preform from the mandrel. While the robot cools the molded preform, the mandrel is available for another molding cycle.

A number of barrier materials having the requisite low permeability to gases such as oxygen and carbon dioxide are useful in preferred embodiments, the choice of barrier material being partly dependent upon the mode or application as described below. Preferred barrier materials for use in barrier coatings include those which fall into two major categories: (1) copolyesters of terephthalic acid, isophthalic acid, and at least one diol having good barrier properties as compared to PET, such as those disclosed in U.S. Patent No. 4,578,295 to Jabarin, and which is commercially available as B-010 (Mitsui Petrochemical Ind. Ltd., Japan); and (2) hydroxy-functional poly(amide-ethers) such as those described in U.S. Patent Nos. 5,089,588 and 5,143,998, poly(hydroxy amide ethers) such as those described in U.S. Patent No. 5,134,218, polyethers such as those described in U.S. Patent No. 5,115,075 and 5,218,075, hydroxy-functional polyethers such as those as described in U.S. Patent No. 5,164,472,

hydroxy-functional poly(ether sulfonamides) such as those described in U.S. Patent No. 5,149,768, poly(hydroxy ester ethers) such as those described in U.S. Patent No. 5,171,820, hydroxy-phenoxyether polymers such as those described in U.S. Patent No. 5,814,373, and poly(hydroxyamino ethers) ("PHAE") such as those described in U.S. Patent No. 5,275,853. The barrier materials described in (1) above are referred to herein by the term "Copolyester Barrier Materials". The compounds described in the patents in (2) above are collectively categorized and referred to herein by the term "Phenoxy-type Thermoplastic" materials. All the patents referenced in this paragraph are hereby incorporated in their entireties into this disclosure by this reference thereto.

Preferred Copolyester Barrier Materials have FDA approval. FDA approval allows for these materials to be used in containers where they are in contact with beverages and the like which are intended for human consumption. To the inventor's knowledge, none of the Phenoxy-type Thermoplastics have FDA approval as of the date of this disclosure. Thus, these materials are preferably used in multi-layered containers in locations that do not directly contact the contents, if the contents are ingestible, or the mouth of the consumer when drinking from the container.

In carrying out preferred methods to form barrier coated preforms and bottles, an initial preform is coated with at least one additional layer of material comprising barrier material, polyesters such as PET, post-consumer or recycled PET (collectively recycled PET), and/or other compatible thermoplastic materials. A coating layer may comprise a single material, a mix or blend of materials (heterogeneous or homogeneous), an interwoven matrix of two or more materials, or a plurality of microlayers (lamellae) comprised of at least two different materials. Initial preforms preferably comprise polyester, preferably virgin materials which are approved by the FDA for being in contact with foodstuffs.

Thus the preforms and containers according to preferred embodiments may exist in several forms, including, but not limited to: virgin PET coated with a layer of barrier material; virgin PET coated with a layer of material comprising alternating microlayers of barrier material and recycled PET; virgin PET coated with a barrier layer which is in turn coated with recycled PET; microlayers of virgin PET and a barrier material coated with a layer of recycled PET; virgin PET having an oxygen scavenger therein coated with recycled PET (RPET), virgin PET having an oxygen scavenger therein coated with recycled PET (RPET) which is coated with a layer of barrier material, or virgin PET coated with recycled PET which is then coated with barrier material. Other such variations and permutations of layer and material combinations are also within the scope of the disclosure and are presently contemplated.

As described previously, preferred barrier materials include Copolyester Barrier Materials and Phenoxy-type Thermoplastics. Other preferred barrier materials include polyamide barrier materials such as Nylon MXD-6 from Mitsubishi Gas Chemical (Japan). Other preferred barrier materials, referred to herein as "Polyamide Blends." Polyamide Blends as used herein shall include those polyamides containing PET or other polyesters, whether such polyester was included by blending, compounding or reacting. Other barrier materials having similar properties may be used in lieu of these barrier materials. For example, the barrier material may take the form of other thermoplastic polymers, such as acrylic resins including polyacrylonitrile polymers, acrylonitrile styrene copolymers, polyamides, polyethylene naphthalate (PEN), PEN copolymers, and PET/PEN blends.



Preferred barrier materials in accordance with embodiments of the present invention have oxygen and carbon dioxide permeabilities which are less than one-third those of polyethylene terephthalate. For example, the Copolyester Barrier Materials preferably exhibit a permeability to oxygen of about 11 cc mil/100 in<sup>2</sup> day and a permeability to carbon dioxide of about 2 cc mil/100 in<sup>2</sup> day. For certain PHAEs, the permeability to oxygen is less than 1 cc mil/100 in<sup>2</sup> day and the permeability to carbon dioxide is 3.9 cc mil/100 in<sup>2</sup> day. The corresponding CO<sub>2</sub> permeability of polyethylene terephthalate, whether in the recycled or virgin form, is about 12-20 cc mil/100 in<sup>2</sup> day.

For embodiments in which the container is heat set during or after blow-molding, it is preferred that the materials which form the container or article can exist in a form which is at least partially crystalline, more preferably primarily crystalline. Accordingly, for such embodiments, preferred barrier materials include PEN, Copolyesters, Polyamide Blends, and Phenoxy-type Thermoplastics which can exist in partially crystalline or primarily crystalline form.

The methods of preferred embodiments provide for a coating to be placed on a preform which is later blown into a bottle. In many cases, such methods are preferable to placing coatings on the bottles themselves. However, in accordance with other preferred embodiments, one or more coating layers may be placed on a bottle or container itself. Preforms are smaller in size and of a more regular shape than the containers blown therefrom, making it simpler to obtain an even and regular coating. Furthermore, bottles and containers of varying shapes and sizes can be made from preforms of similar size and shape. Thus, the same equipment and processing can be used to produce preforms to form several different kinds of containers. The blow-molding may take place soon after molding, or preforms may be made and stored for later blow-molding. If the preforms are stored prior to blow-molding, their smaller size allows them to take up less space in storage.

Even though it is preferable to form containers from coated preforms as opposed to coating containers themselves, they have generally not been used because of the difficulties involved in making containers from coated or multi-layer preforms. One step where the greatest difficulties arise is during the blow-molding process to form the container from the preform. During this process, defects such as delamination of the layers, cracking or crazing of the coating, uneven coating thickness, and discontinuous coating or voids can result. These difficulties can be overcome by using suitable barrier materials and coating the preforms in a manner that allows for good adhesion between the layers.

Thus, one aspect is the choice of a suitable barrier material, for those embodiments which include barrier materials. When a suitable barrier material is used, the coating sticks directly to the preform without any significant delamination, and will continue to stick as the preform is blow-molded into a bottle and afterwards. Use of a suitable barrier material also helps to decrease the incidence of cosmetic and structural defects which can result from blow-molding containers as described above.

It should be noted that although most of the discussion, drawings, and examples of making coated preforms deal with two layer preforms or bottles incorporating barrier layers, such discussion is not intended to limit the present invention to two layer barrier articles. The disclosure should be read to include, incorporate and describe articles

having one or more layers, each layer of which is independently selected from the materials disclosed herein and materials similar thereto.

The two layer barrier containers and preforms according to preferred embodiments are suitable for many uses and are cost-effective because of the economy of materials and processing steps. However, in some circumstances and for some applications, preforms consisting of more than two layers may be desired. Use of three or more layers allows for incorporation of materials such as recycled PET, which is generally less expensive than virgin PET or the preferred barrier materials. Thus, it is contemplated that all of the methods for producing the barrier-coated preforms which are disclosed herein and all other suitable methods for making such preforms may be used, either alone or in combination to produce barrier-coated preforms and containers comprised of two or more layers.

In another aspect of the present invention, preforms and containers, including those which incorporate RPET, may be treated with additional external coatings through dip or spray processes. The materials dipped or sprayed upon the containers or preforms include, but are not limited to, solutions or dispersions of Phenoxy-type thermoplastics.

Referring to FIGURE 1, a preferred uncoated preform 30 is depicted. The preform is preferably made of an FDA approved material such as virgin PET and can be of any of a wide variety of shapes and sizes. The preform shown in FIGURE 1 is of the type which will form a 16 oz. carbonated beverage bottle that requires an oxygen and carbon dioxide barrier, but as will be understood by those skilled in the art, other preform configurations can be used depending upon the desired configuration, characteristics and use of the final article. The uncoated preform 30 may be made by injection molding as is known in the art or by methods disclosed herein.

Referring to FIGURE 2, a cross-section of the preferred uncoated preform 30 of FIGURE 1 is depicted. The uncoated preform 30 has a neck portion 32 and a body portion 34, formed monolithically (i.e., as a single, or unitary, structure). Advantageously, the monolithic arrangement of the preform, when blow-molded into a bottle, provides greater dimensional stability and improved physical properties in comparison to a preform constructed of separate neck and body portions, which are bonded together.

The neck portion 32 begins at the opening 36 to the interior of the preform 30 and extends to and includes the support ring 38. The neck portion 32 is further characterized by the presence of the threads 40, which provide a way to fasten a cap for the bottle produced from the preform 30. The body portion 34 is an elongated and cylindrically shaped structure extending down from the neck portion 32 and culminating in the rounded end cap 42. The preform thickness 44 will depend upon the overall length of the preform 30 and the wall thickness and overall size of the resulting container.

Referring to FIGURE 3, a cross-section of one type of barrier-coated preform 50 having features in accordance with a preferred embodiment is disclosed. The barrier-coated preform 50 has a neck portion 32 and a body portion 34 as in the uncoated preform 30 in FIGURES 1 and 2. The barrier coating layer 52 is disposed about the entire surface of the body portion 34, terminating at the bottom of the support ring 38. A barrier coating layer 52 in the embodiment shown in the figure does not extend to the neck portion 32, nor is it present on the interior surface 54 of the preform which is preferably made of an FDA approved material such as PET. The barrier coating layer 52 may

comprise either a single material or several microlayers of at least two materials. The overall thickness 56 of the preform is equal to the thickness of the initial preform plus the thickness 58 of the barrier layer, and is dependent upon the overall size and desired coating thickness of the resulting container. By way of example, the wall of the bottom portion of the preform may have a thickness of 3.2 millimeters; the wall of the neck, a cross-sectional dimension of about 3 millimeters; and the barrier material applied to a thickness of about 0.3 millimeters.

Referring to FIGURE 4, a preferred embodiment of a coated preform 60 is shown in cross-section. The primary difference between the coated preform 60 and the coated preform 50 in FIGURE 3 is the relative thickness of the two layers in the area of the end cap 42. In coated preform 50, the barrier layer 52 is generally thinner than the thickness of the initial preform throughout the entire body portion of the preform. In coated preform 60, however, the barrier coating layer 52 is thicker at 62 near the end cap 42 than it is at 64 in the wall portion 66, and conversely, the thickness of the inner polyester layer is greater at 68 in the wall portion 66 than it is at 70, in the region of the end cap 42. This preform design is especially useful when the barrier coating is applied to the initial preform in an overmolding process to make the coated preform, as described below, where it presents certain advantages including that relating to reducing molding cycle time. These advantages will be discussed in more detail below. The barrier coating layer 52 may be homogeneous or it may be comprised of a plurality of microlayers.

The barrier preforms and containers can have layers which have a wide variety of relative thicknesses. In view of the present disclosure, the thickness of a given layer and of the overall preform or container, whether at a given point or over the entire container, can be chosen to fit a coating process or a particular end use for the container. Furthermore, as discussed above in regard to the barrier coating layer in FIGURE 3, the barrier coating layer in the preform and container embodiments disclosed herein may comprise a single material or several microlayers of two or more materials.

After a barrier-coated preform, such as that depicted in FIGURE 3, is prepared by a method and apparatus such as those discussed in detail below, it is subjected to a stretch blow-molding process. Referring to FIGURE 5, in this process a barrier-coated preform 50 is placed in a mold 80 having a cavity corresponding to the desired container shape. The barrier-coated preform is then heated and expanded by stretching and by air forced into the interior of the preform 50 to fill the cavity within the mold 80, creating a barrier-coated container 82. The blow molding operation normally is restricted to the body portion 34 of the preform with the neck portion 32 including the threads, pilfer ring, and support ring retaining the original configuration as in the preform.

Referring to FIGURE 6, there is disclosed an embodiment of barrier coated container 82 in accordance with a preferred embodiment, such as that which might be made from blow molding the barrier coated preform 50 of Figure 3. The container 82 has a neck portion 32 and a body portion 34 corresponding to the neck and body portions of the barrier-coated preform 50 of Figure 3. The neck portion 32 is further characterized by the presence of the threads 40 which provide a way to fasten a cap onto the container.

The barrier coating 84 covers the exterior of the entire body portion 34 of the container 82, stopping just below the support ring 38. The interior surface 86 of the container, which is made of an FDA-approved material,

preferably PET, remains uncoated so that only the interior surface 86 is in contact with beverages or foodstuffs. In one preferred embodiment that is used as a carbonated beverage container, the thickness 87 of the barrier coating is preferably 0.020-0.060 inch, more preferably 0.030-0.040 inch; the thickness 88 of the PET layer is preferably 0.080-0.160 inch, more preferably 0.100-0.140 inch; and the overall wall thickness 90 of the barrier-coated container 82 is preferably 0.140-0.180 inch, more preferably 0.150-0.170 inch. Preferably, on average, the overall wall thickness 90 of the container 82 derives the majority of its thickness from the inner PET layer.

FIGURE 7 illustrates a preferred type of mold for use in methods which utilize overmolding. The mold comprises two halves, a cavity half 92 and a mandrel half 94. The cavity half 92 comprises a cavity in which an uncoated preform is placed. The preform is held in place between the mandrel half 94, which exerts pressure on the top of the preform and the ledge 96 of the cavity half 92 on which the support ring 38 rests. The neck portion 32 of the preform is thus sealed off from the body portion of the preform. Inside the preform is the mandrel 98. As the preform sits in the mold, the body portion of the preform is completely surrounded by a void space 100. The preform, thus positioned, acts as an interior die mandrel in the subsequent injection procedure, in which the melt of the overmolding material is injected through the gate 102 into the void space 100 to form the coating. The melt, as well as the uncoated preform, is cooled by fluid circulating within channels 104 and 106 in the two halves of the mold. Preferably the circulation in channels 104 is completely separate from the circulation in the channels 106.

FIGURES 8 and 9 are a schematic of a portion of the preferred type of apparatus to make coated preforms in accordance with a preferred embodiment. The apparatus is an injection molding system designed to make one or more uncoated preforms and subsequently coat the newly-made preforms by over-injection of a barrier material. FIGURES 8 and 9 illustrate the two halves of the mold portion of the apparatus which will be in opposition in the molding machine. The alignment pegs 110 in FIGURE 8 fit into their corresponding receptacles 112 in the other half of the mold.

The mold half depicted in FIGURE 9 has several pairs of mold cavities, each cavity being similar to the mold cavity depicted in FIGURE 7. The mold cavities are of two types: first injection preform molding cavities 114 and second injection preform coating cavities 120. The two types of cavities are equal in number and are preferably arranged so that all cavities of one type are on the same side of the injection block 124 as bisected by the line between the alignment peg receptacles 112. This way, every preform molding cavity 114 is 180° away from a preform coating cavity 120.

The mold half depicted in FIGURE 8 has several mandrels 98, one for each mold cavity (114 and 120). When the two halves which are FIGURES 8 and 9 are put together, a mandrel 98 fits inside each cavity and serves as the mold for the interior of the preform for the preform molding cavities 114 and as a centering device for the uncoated preforms in preform coating cavities 120. The mandrels 98 are mounted on a turntable 130 which rotates 180° about its center so that a mandrel 98 originally aligned with a preform molding cavity 114 will, after rotation, be aligned with a preform coating cavity 120, and vice-versa. As described in greater detail below, this type of setup allows a preform to be molded and then coated in a two-step process using the same piece of equipment.

It should be noted that the drawings in FIGURES 8 and 9 are merely illustrative. For instance, the drawings depict an apparatus having three molding cavities 114 and three coating cavities 120 (a 3/3 cavity machine). However, the machines may have any number of cavities, as long as there are equal numbers of molding and coating cavities, for example 12/12, 24/24, 48/48 and the like. The cavities may be arranged in any suitable manner. These and other minor alterations are contemplated as part of this disclosure.

The two mold halves depicted in FIGURES 10 and 11 illustrate an embodiment of a mold of a 48/48 cavity machine as discussed for FIGURES 8 and 9. Referring to FIGURE 12 there is shown a perspective view of a mold of the type for an overmolding (inject-over-inject) process in which the mandrels 98 are partially located within the cavities 114 and 120. The arrow shows the movement of the movable mold half 142, on which the mandrels 98 lie, as the mold closes.

FIGURE 13 shows a perspective view of a mold of the type used in an overmolding process, wherein the mandrels 98 are fully withdrawn from the cavities 114 and 120. The arrow indicates that the turntable 130 rotates 180° to move the mandrels 98 from one cavity to the next. On the stationary half 144, the cooling for the preform molding cavity 114 is separate from the cooling for the preform coating cavity 120. Both of these are separate from the cooling for the mandrels 98 in the movable half.

Referring to FIGURE 14 there is shown a preferred three-layer preform 132. This embodiment of coated preform is preferably made by placing two coating layers 134 and 136 on a preform 30 such as that shown in FIGURE 1.

With next reference to FIGURE 15, a preferred embodiment of a mold mandrel 298 and associated cavity 300 are shown. Cooling tubes 302 are formed in a spiral fashion just below the surface 304 of the mold cavity 300. A gate area 308 of the cavity 300 is defined near a gate 308 and an insert 310 of a material with especially high heat transfer properties is disposed in the cavity at the gate area 306. Thus, the injected preform's gate area/base end 314 is cooled especially quickly.

The mandrel 298 is hollow and has a wall 320 of generally uniform thickness. A bubbler cooling arrangement 330 is disposed within the hollow mandrel 298 and comprises a core tube 332 located centrally within the mandrel 298 which delivers chilled coolant C directly to a base end 322 of the mandrel 298. Coolant C works its way up the mandrel from the base end 322 and exits through an output line 334. The core tube is held in place by ribs 336 extending between the tube and the mandrel wall 320.

The body mold 404 has several cooling tubes 302 through which a chilled fluid, preferably water, is circulated. The neck finish mold 402 has several tubes 403 in which a fluid circulates. The fluid and circulation of tubes 403 and cooling tubes 302 are separate and independent. The coolant C circulating through the core section 400 is also separate from both tubes 403 and cooling tubes 302. However, a single coolant source may provide the coolant C for both core section 400 and cooling tubes 302 within the body portion 404 of the mold.

The thermal isolation of the body mold 404, neck finish mold 402 and core section 400 is achieved by use of inserts 406 having low thermal conductivity. However, materials having low thermal conductivity should not be used

on the molding surfaces which contact the preform. Examples of preferred low thermal conductivity materials include heat-treated tool steel (e.g. P-20, H-13, Stainless etc.), polymeric inserts of filled polyamides, nomex, air gaps and minimum contact shut-off surfaces.

In this independent fluid circuit through tubes 403, the fluid would be warmer than that used in the portions of the mold used to form non-crystalline portions of the preform. Preferred fluids include water, silicones, and oils. In another embodiment, the portions of the mold which forms the crystalline portions of the preform, (corresponding to neck finish mold 402) contains a heating apparatus placed in the neck, neck finish, and/or neck cylinder portions of the mold so as to maintain the higher temperature (slower cooling) needed to promote crystallinity of the material during cooling. Such a heating apparatus includes but is not limited to heating coils, heating probes, and electric heaters,

Referring also to FIGURES 16 and 17, an air insertion system 340 is shown formed at a joint 342 between members of the mold cavity 300. A notch 344 is formed circumferentially around the cavity 300. The notch 344 is sufficiently small that substantially no molten plastic will enter during melt injection. An air line 350 connects the notch 344 to a source of air pressure and a valve regulates the supply of air to the notch 344. During melt injection, the valve is closed. When injection is complete, the valve is opened and pressurized air A is supplied to the notch 344 in order to defeat a vacuum that may form between an injected preform and the cavity wall 304. Additionally, similar air insertion systems 340 may be utilized in other portions of the mold, such as the thread area, for example but without limitation.

The preferred method and apparatus for making barrier coated preforms is discussed in more detail below. Because the methods and apparatus are especially preferred for use in forming barrier coated bottles comprising certain preferred materials, the physical characteristics, identification, preparation and enhancement of the preferred materials is discussed prior to the preferred methods and apparatus for working with the materials.

#### A. Physical Characteristics of Preferred Barrier Materials

Preferred barrier materials preferably exhibit several physical characteristics which allow for the barrier coated bottles and articles according to preferred embodiments to be able to withstand processing and physical stresses in a manner similar or superior to that of uncoated PET articles, in addition to producing articles which are cosmetically appealing and have excellent barrier properties.

Adhesion is the union or sticking together of two surfaces. The actual interfacial adhesion is a phenomenon which occurs at the microscopic level. It is based upon molecular interactions and depends upon chemical bonding, van der Waals forces and other intermolecular attractive forces at the molecular level.

Good adhesion between the barrier layer and the PET layer is especially important when the article is a barrier bottle made by blow-molding a preform. If the materials adhere well, then they will act as one unit when they are subjected to a blow molding process and as they are subjected to stresses when existing in the form of a container. Where the adhesion is poor, delamination results either over time or under physical stress such as squeezing the container or the container jostling during shipment. Delamination is not only unattractive from a commercial standpoint, it may be evidence of a lack of structural integrity of the container. Furthermore, good adhesion means

that the layers will stay in close contact when the container is expanded during the molding process and will move as one unit. When the two materials act in such a manner, it is less likely that there will be voids in the coating, thus allowing a thinner coating to be applied. The barrier materials preferably adhere sufficiently to PET such that the barrier layer cannot be easily pulled apart from the PET layer at 22°C.

5 The glass transition temperature ( $T_g$ ) is defined as the temperature at which a non-crystallizable polymer undergoes the transformation from a soft rubber state to a hard elastic polymer glass. In a range of temperatures above its  $T_g$ , a material will become soft enough to allow it to flow readily when subjected to an external force or pressure, yet not so soft that its viscosity is so low that it acts more like a liquid than a pliable solid. The temperature range above  $T_g$  is the preferred temperature range for performing a blow-molding process, as the material is soft  
10 enough to flow under the force of the air blown into the preform to fit the mold but not so soft that it breaks up or becomes uneven in texture. Thus, when materials have similar glass transition temperatures, they will have similar preferred blowing temperature ranges, allowing the materials to be processed together without compromising the performance of either material.

In the blow-molding process to produce bottle from a preform, as is known in the art, the preform is heated  
15 to a temperature slightly above the  $T_g$  of the preform material so that when air is forced into the preform's interior, it will be able to flow to fill the mold in which it is placed. If one does not sufficiently heat the preform and uses a temperature below the  $T_g$ , the preform material will be too hard to flow properly, and would likely crack, craze, or not expand to fill the mold. Conversely, if one heats the preform to a temperature well above the  $T_g$ , the material would likely become so soft that it would not be able to hold its shape and would process improperly.

20 If a barrier coating material has a  $T_g$  similar to that of PET, it will have a blowing temperature range similar to PET. Thus, if a PET preform is coated with such a barrier material, a blowing temperature can be chosen that allows both materials to be processed within their preferred blowing temperature ranges. If the barrier coating were to have a  $T_g$  dissimilar to that of PET, it would be difficult, if not impossible, to choose a blowing temperature suitable for both materials. When the barrier coating materials have a  $T_g$  similar to PET, the coated preform behaves during  
25 blow molding as if it were made of one material, expanding smoothly and creating a cosmetically appealing container with an even thickness and uniform coating of the barrier material where it is applied.

The glass transition temperature of PET occurs in a window of about 75-85°C, depending upon how the PET has been processed previously. The  $T_g$  for preferred barrier materials is preferably 55 to 140°C, more preferably 90 to 110°C.

30 Another factor which has an impact on the performance of barrier preforms during blow molding is the state of the material. The preferred barrier materials of preferred embodiments are amorphous rather than crystalline. This is because materials in an amorphous state are easier to form into bottles and containers by use of a blow molding process than materials in a crystalline state. PET can exist in both crystalline and amorphous forms. However, in preferred embodiments it is highly preferred that the crystallinity of the PET be minimized and the amorphous state  
35 maximized in order to create a semi-crystalline state which, among other things, aids interlayer adhesion and in the

blow molding process. A PET article formed from a melt of PET, as in injection molding, can be guided into a semi-crystalline form by cooling the melt at a high rate, fast enough to quench the crystallization process, freezing the PET in a mostly amorphous state. Additionally, use of "high IPA PET" as described earlier herein will allow easier quenching of the crystallization process because it crystallizes at a lower rate than homopolymer PET.

5        Intrinsic viscosity and melt index are two properties which are related to a polymer's molecular weight. These properties give an indication as to how materials will act under various processing conditions, such as injection molding and blow molding processes.

Barrier materials for use in the articles and methods according to preferred embodiments have an intrinsic viscosity of preferably 0.70-0.90 dl/g, more preferably 0.74-0.87 dl/g, most preferably 0.84-0.85 dl/g and a melt index  
10    of preferably 5-30, more preferably 7-12, most preferably 10.

Barrier materials preferably have tensile strength and creep resistance similar to PET. Similarity in these physical properties allows the barrier coating to act as more than simply a gas barrier. A barrier coating having physical properties similar to PET acts as a structural component of the container, allowing the barrier material to displace some of the polyethylene terephthalate in the container without sacrificing container performance.  
15    Displacement of PET allows for the resulting barrier-coated containers to have physical performance and characteristics similar to their uncoated counterparts without a substantial change in weight or size. It also allows for any additional cost from adding the barrier material to be defrayed by a reduction in the cost per container attributed to PET.

Similarity in tensile strength between PET and the barrier coating materials helps the container to have  
20    structural integrity. This is especially important if some PET is displaced by barrier material. Barrier-coated bottles and containers having features in accordance with preferred embodiments are able to withstand the same physical forces as an uncoated container, allowing, for example, barrier-coated containers to be shipped and handled in the customary manner of handling uncoated PET containers. If the barrier-coating material were to have a tensile strength substantially lower than that of PET, a container having some PET displaced by barrier material would likely not be  
25    able to withstand the same forces as an uncoated container.

Similarity in creep resistance between PET and the barrier coating materials helps the container to retain its shape. Creep resistance relates to the ability of a material to resist changing its shape in response to an applied force. For example, a bottle which holds a carbonated liquid needs to be able to resist the pressure of dissolved gas pushing outward and retain its original shape. If the barrier coating material were to have a substantially lower resistance to  
30    creep than PET in a container, the resulting container would be more likely to deform over time, reducing the shelf-life of the product.

For applications where optical clarity is of importance, preferred barrier materials have an index of refraction similar to that of PET. When the refractive index of the PET and the barrier coating material are similar, the preforms and, perhaps more importantly, the containers blown therefrom are optically clear and, thus, cosmetically appealing for  
35    use as a beverage container where clarity of the bottle is frequently desired. If, however, the two materials have



substantially dissimilar refractive indices when they are placed in contact with each other, the resulting combination will have visual distortions and may be cloudy or opaque, depending upon the degree of difference in the refractive indices of the materials.

Polyethylene terephthalate has an index of refraction for visible light within the range of about 1.40 to 1.75, depending upon its physical configuration. When made into preforms, the refractive index is preferably within the range of about 1.55 to 1.75, and more preferably in the range of 1.55-1.65. After the preform is made into a bottle, the wall of the final product, may be characterized as a biaxially-oriented film since it is subject to both hoop and axial stresses in the blow molding operation. Blow molded PET generally exhibits a refractive index within the range of about 1.40 to 1.75, usually about 1.55 to 1.75, depending upon the stretch ratio involved in the blow molding operation. For relatively low stretch ratios of about 6:1, the refractive index will be near the lower end, whereas for high stretch ratios, about 10:1, the refractive index will be near the upper end of the aforementioned range. It will be recognized that the stretch ratios referred to herein are biaxial stretch ratios resulting from and include the product of the hoop stretch ratio and the axial stretch ratio. For example, in a blow molding operation in which the final preform is enlarged by a factor of 2.5 in the axial direction and a factor of 3.5 diametrically, the stretch ratio will be about 8.75 (2.5 x 3.5).

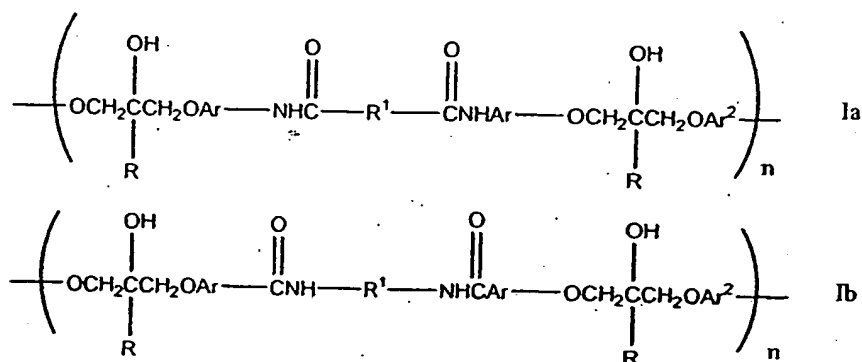
Using the designation  $n_1$  to indicate the refractive index for PET and  $n_2$  to indicate the refractive index for the barrier material, the ratio between the values  $n_1$  and  $n_2$  is preferably 0.8-1.3, more preferably 1.0-1.2, most preferably 1.0-1.1. As will be recognized by those skilled in the art, for the ratio  $n_1/n_2 = 1$  the distortion due to refractive index will be at a minimum, because the two indices are identical. As the ratio progressively varies from one, however, the distortion increases progressively.

#### B. Preferred Barrier Coating Materials and Their Preparation

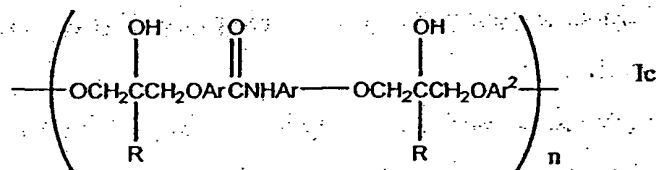
The preferred barrier coating materials for use in the articles and methods described herein include Phenoxy-type Thermoplastic materials, copolyesters of terephthalic acid, isophthalic acid, and at least one diol having good barrier properties as compared to PET (Copolyester Barrier Materials), polyamides, Polyamide Blends, PEN, PEN copolymers, PEN/PET blends, and combinations thereof. Preferably, the Phenoxy-type Thermoplastics used as barrier materials are one of the following types:

hydroxy-functional poly(amide ethers) having repeating units represented by any one of the Formulae Ia, Ib or

Ic:

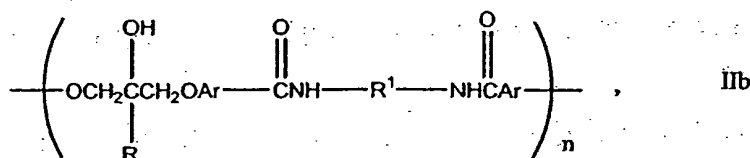
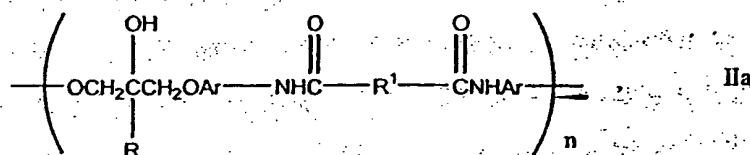


or



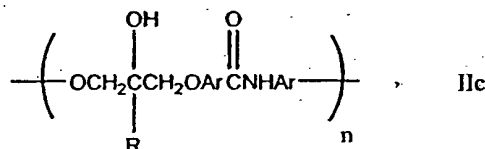
poly(hydroxy amide ethers) having repeating units represented independently by any one of the Formulae IIa,

5 IIb or IIc:

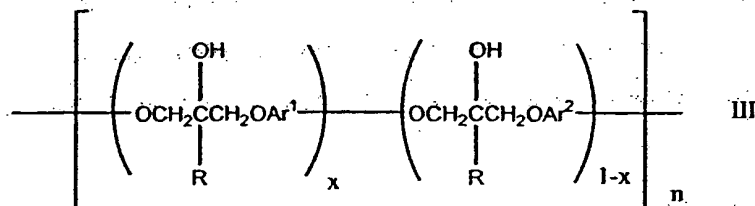


10

or

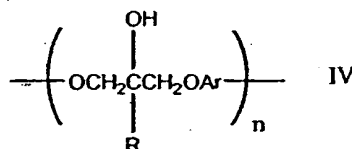


amide- and hydroxymethyl-functionalized polyethers having repeating units represented by Formula III:

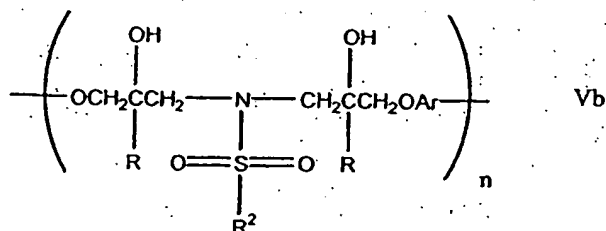
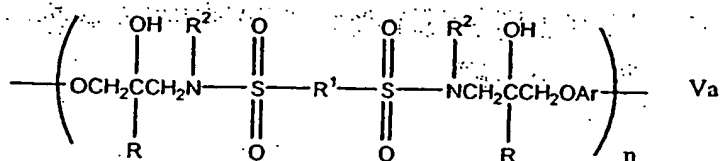


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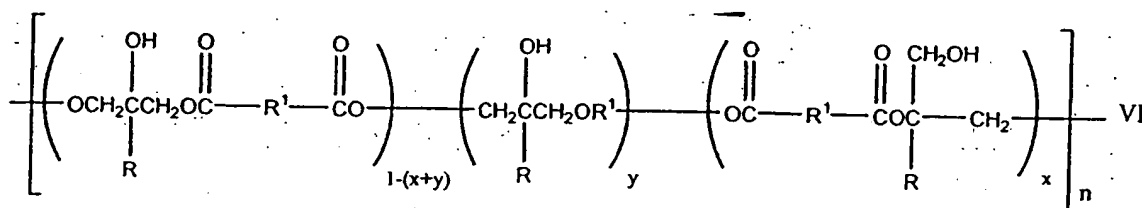
hydroxy-functional polyethers having repeating units represented by Formula IV:



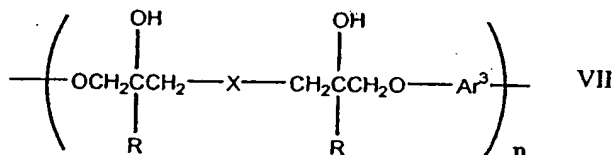
hydroxy-functional poly(ether sulfonamides) having repeating units represented by Formulae Va or Vb:



poly(hydroxy ester ethers) having repeating units represented by Formula VI:

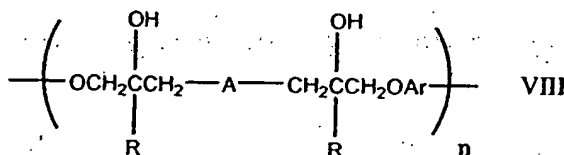


hydroxy-phenoxyether polymers having repeating units represented by Formula VII:



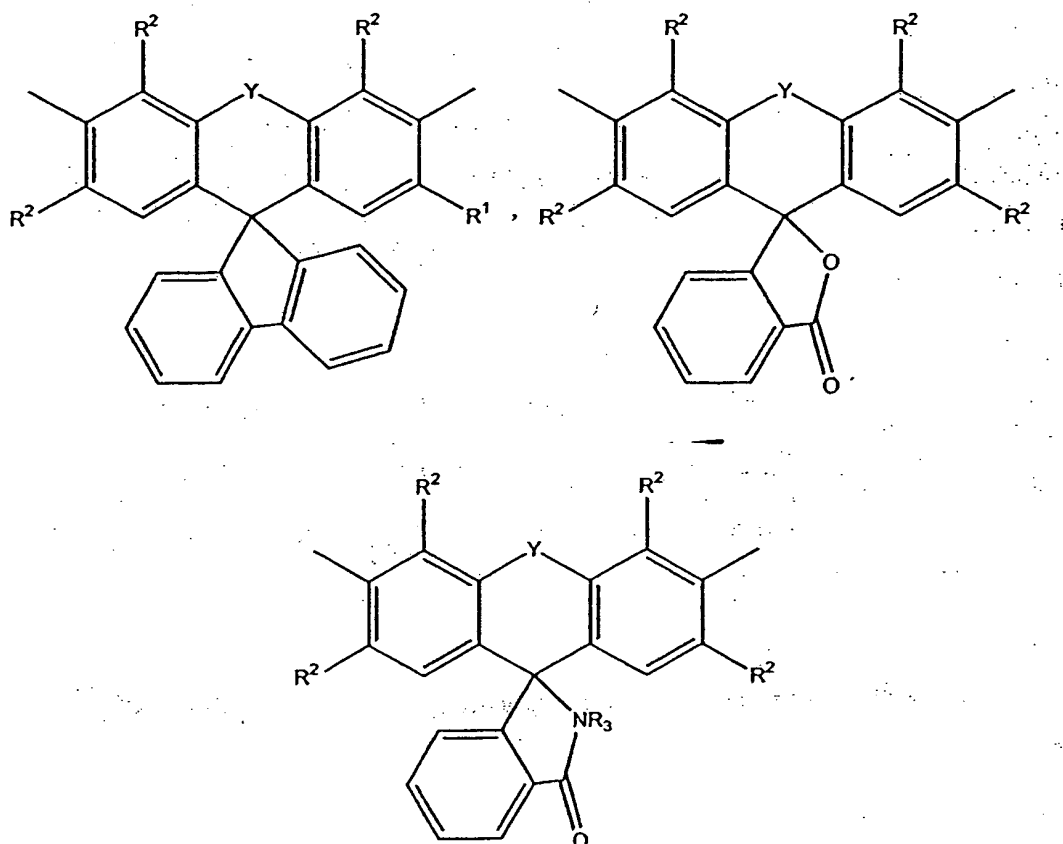
and

poly(hydroxyamino ethers) having repeating units represented by Formula VIII:



wherein each Ar individually represents a divalent aromatic moiety, substituted divalent aromatic moiety or heteroaromatic moiety, or a combination of different divalent aromatic moieties, substituted aromatic moieties or heteroaromatic moieties; R is individually hydrogen or a monovalent hydrocarbyl moiety; each Ar<sub>1</sub> is a divalent aromatic moiety or combination of divalent aromatic moieties bearing amide or hydroxymethyl groups; each Ar<sub>2</sub> is the same or different than Ar and is individually a divalent aromatic moiety, substituted aromatic moiety or heteroaromatic moiety or a combination of different divalent aromatic moieties, substituted aromatic moieties or heteroaromatic moieties; R<sub>1</sub> is individually a predominantly hydrocarbylene moiety, such as a divalent aromatic moiety, substituted divalent aromatic moiety, divalent heteroaromatic moiety, divalent alkylene moiety, divalent substituted alkylene moiety or divalent heteroalkylene moiety or a combination of such moieties; R<sub>2</sub> is individually a monovalent hydrocarbyl moiety; A is an amine moiety or a combination of different amine moieties; X is an amine, an arylene, an

arylenedisulfonamido or an arylenedicarboxy moiety or combination of such moieties; and  $Ar_3$  is a "cardo" moiety represented by any one of the Formulae:



5

wherein Y is nil, a covalent bond, or a linking group, wherein suitable linking groups include, for example, an oxygen atom, a sulfur atom, a carbonyl atom, a sulfonyl group, or a methylene group or similar linkage; n is an integer from about 10 to about 1000; x is 0.01 to 1.0; and y is 0 to 0.5.

The term "predominantly hydrocarbylene" means a divalent radical that is predominantly hydrocarbon, but which optionally contains a small quantity of a heteroatomic moiety such as oxygen, sulfur, imino, sulfonyl, sulfoxyl, and the like.

The hydroxy-functional poly(amide ethers) represented by Formula I are preferably prepared by contacting an N,N'-bis(hydroxyphenylamido)alkane or arene with a diglycidyl ether as described in U.S. Patent Nos. 5,089,588 and 5,143,998.

The poly(hydroxy amide ethers) represented by Formula II are prepared by contacting a bis(hydroxyphenylamido)alkane or arene, or a combination of 2 or more of these compounds, such as N,N'-bis(3-hydroxyphenyl) adipamide or N,N'-bis(3-hydroxyphenyl)glutaramide, with an epihalohydrin as described in U.S. Patent No. 5,134,218.

The amide- and hydroxymethyl-functionalized polyethers represented by Formula III can be prepared, for example, by reacting the diglycidyl ethers, such as the diglycidyl ether of bisphenol A, with a dihydric phenol having pendant amido, N-substituted amido and/or hydroxyalkyl moieties, such as 2,2-bis(4-hydroxyphenyl)acetamide and

20

3,5-dihydroxybenzamide. These polyethers and their preparation are described in U.S. Patent Nos. 5,115,075 and 5,218,075.

The hydroxy-functional polyethers represented by Formula IV can be prepared, for example, by allowing a diglycidyl ether or combination of diglycidyl ethers to react with a dihydric phenol or a combination of dihydric phenols using the process described in U.S. Patent No. 5,164,472. Alternatively, the hydroxy-functional polyethers are obtained by allowing a dihydric phenol or combination of dihydric phenols to react with an epihalohydrin by the process described by Reinking, Barnabeo and Hale in the Journal of Applied Polymer Science, Vol. 7, p. 2135 (1963).

The hydroxy-functional poly(ether sulfonamides) represented by Formula V are prepared, for example, by polymerizing an N,N'-dialkyl or N,N'-diaryldisulfonamide with a diglycidyl ether as described in U.S. Patent No. 5,149,768.

The poly(hydroxy ester ethers) represented by Formula VI are prepared by reacting diglycidyl ethers of aliphatic or aromatic diacids, such as diglycidyl terephthalate, or diglycidyl ethers of dihydric phenols with, aliphatic or aromatic diacids such as adipic acid or isophthalic acid. These polyesters are described in U.S. Patent No. 5,171,820.

The hydroxy-phenoxyether polymers represented by Formula VII are prepared, for example, by contacting at least one dinucleophilic monomer with at least one diglycidyl ether of a cardo bisphenol, such as 9,9-bis(4-hydroxyphenyl)fluorene, phenolphthalein, or phenolphthalimidine or a substituted cardo bisphenol, such as a substituted bis(hydroxyphenyl)fluorene, a substituted phenolphthalein or a substituted phenolphthalimidine under conditions sufficient to cause the nucleophilic moieties of the dinucleophilic monomer to react with epoxy moieties to form a polymer backbone containing pendant hydroxy moieties and ether, imino, amino, sulfonamido or ester linkages. These hydroxy-phenoxyether polymers are described in U.S. Patent No. 5,184,373.

The poly(hydroxyamino ethers) ("PHAE" or polyetheramines) represented by Formula VIII are prepared by contacting one or more of the diglycidyl ethers of a dihydric phenol with an amine having two amine hydrogens under conditions sufficient to cause the amine moieties to react with epoxy moieties to form a polymer backbone having amine linkages, ether linkages and pendant hydroxyl moieties. These compounds are described in U.S. Patent No. 5,275,853.

Phenoxy-type Thermoplastics of Formulae I-VIII may be acquired from Dow Chemical Company (Midland, Michigan U.S.A.).

The Phenoxy-type Thermoplastics commercially available from Phenoxy Associates, Inc. are also suitable for use. These hydroxy-phenoxyether polymers are the condensation reaction products of a dihydric polynuclear phenol, such as bisphenol A, and an epihalohydrin and have the repeating units represented by Formula IV wherein Ar is an isopropylidene diphenylene moiety. The process for preparing these is described in U.S. Patent No. 3,305,528, incorporated herein by reference in its entirety.

Especially preferred hydroxy-phenoxyether polymers are the poly(hydroxyamino ethers) ("PHAE" or polyetheramines) represented by Formula VIII, sold as BLOX resins from The Dow Chemical Company, including, but not limited to BLOX 0005 and BLOX 0003.

Examples of preferred Copolyester Barrier Materials and a process for their preparation is described in U.S. Patent No. 4,578,295 to Jabarin. They are generally prepared by heating a mixture of at least one reactant selected from isophthalic acid, terephthalic acid and their C<sub>1</sub> to C<sub>4</sub> alkyl esters with 1,3 bis(2-hydroxyethoxy)benzene and ethylene glycol. Optionally, the mixture may further comprise one or more ester-forming dihydroxy hydrocarbon and/or bis(4-β-hydroxyethoxyphenyl)sulfone. Especially preferred Copolyester Barrier Materials are available from Mitsui Petrochemical Ind. Ltd. (Japan) as B-010, B-030 and others of this family.

Examples of preferred polyamide barrier materials include MXD-6 from Mitsubishi Gas Chemical (Japan). Other preferred barrier materials are "Polyamide Blends" which are blends of polyamide and polyester containing preferably about 1-40% of polyester in polyamide, about 1-40% polyamide in polyester, or about 1-40% of the about 1-40% polyamide in polyester blend in polyamide. These blends more preferably include about 5-30% of the lesser component. The blends may incorporate a compatibilizer such as dianhydrides of Tetracarboxylic acids, or other such compatibilizers such as are disclosed in European Patent Application No. 964,031. One preferred dianhydride is pyromellitic dianhydride (PMDA). It may be used to form blends or it may be incorporated into a single polymer to increase its ability to adhere to other layers of materials. The polyester used in Polyamide Blends is preferably PET, more preferably high IPA PET. Recycled PET may also be used such as to save materials costs or increase the recycled content of the article. If a Polyamide Blend is to be in contact with food, however, virgin materials are preferred. These materials are preferably made by adding the component present in smaller quantity to the polycondensation mixture of the polymer present in larger quantity. "Polyamide Blends" as used herein shall include all of the aforementioned types of blends, whether such blends were made by reacting or compounding of the materials.

Other preferred barrier materials include polyethylene naphthalate (PEN), PEN copolyester, and PET/PEN blends. PEN materials can be purchased from Shell Chemical Company.

### C. Preparation of Polyesters

Polyesters and methods for their preparation (including the specific monomers employed in their formation, their proportions, polymerization temperatures, catalysts and other conditions) are well-known in the art and reference is made thereto for the purposes herein. For purposes of illustration and not limitation, reference is particularly made to pages 1-62 of Volume 12 of the Encyclopedia of Polymer Science and Engineering, 1988 revision, John Wiley & Sons.

Typically, polyesters are derived from the reaction of a di- or polycarboxylic acid with a di- or polyhydric alcohol. Suitable di- or polycarboxylic acids include polycarboxylic acids and the esters and anhydrides of such acids, and mixture thereof. Representative carboxylic acids include phthalic, isophthalic, adipic, azelaic, terephthalic, oxalic, malonic, succinic, glutaric, sebacic, and the like. Dicarboxylic components are preferred. Terephthalic acid is most commonly employed and preferred in the preparation of polyester films. α,β-Unsaturated di- and polycarboxylic acids (including esters or anhydrides of such acids and mixtures thereof) can be used as partial replacement for the saturated carboxylic components. Representative α,β-unsaturated di- and polycarboxylic acids include maleic, fumaric, aconitic, itaconic, mesaconic, citraconic, monochloromaleic and the like.

Typical di- and polyhydric alcohols used to prepare the polyester are those alcohols having at least two hydroxy groups, although minor amounts of alcohol having more or less hydroxy groups may be used. Dihydroxy alcohols are preferred. Dihydroxy alcohols conventionally employed in the preparation of polyesters include diethylene glycol; dipropylene glycol; ethylene glycol; 1,2-propylene glycol; 1,4-butanediol; 1,4-pentanediol; 1,5-hexanediol; 1,4-cyclohexanedimethanol and the like with 1,2-propylene glycol being preferred. Mixtures of the alcohols can also be employed. The di- or polyhydric alcohol component of the polyester is usually stoichiometric or in slight excess with respect to the acid. The excess of the di- or polyhydric alcohol will seldom exceed about 20 to 25 mole percent and usually is between about 2 and about 10 mole percent.

The polyester is generally prepared by heating a mixture of the di- or polyhydric alcohol and the di- or polycarboxylic component in their proper molar ratios at elevated temperatures, usually between about 100°C and 250°C for extended periods of time, generally ranging from 5 to 15 hours. Polymerization inhibitors such as t-butylcatechol may advantageously be used.

PET, the preferred polyester, which is commonly made by condensation of terephthalic acid and ethylene glycol, may be purchased from Dow Chemical Company (Midland, Michigan), and Allied Signal Inc. (Baton Rouge, LA), among many others.

Preferably, the PET used is that in which isophthalic acid (IPA) is added during the manufacture of the PET to form a copolymer. The amount of IPA added is preferably 2-10% by weight, more preferably 3-8% by weight, most preferably 4-5% by weight. The most preferred range is based upon current FDA regulations which currently do not allow for PET materials having an IPA content of more than 5% to be in contact with food or drink. High-IPA PET (PET having more than about 2% IPA by weight) can be made as discussed above, or purchased from a number of different manufacturers, for instance PET with 4.8% IPA may be purchased from SKF (Italy) and 10% IPA PET may be purchased from INCA (Dow Europe).

Additionally, if a barrier material containing polyamide is chosen, it is preferred to use the Polyamide Blends.

#### **D. Other Materials to Enhance Barrier Properties**

The materials noted herein, including base materials, such as PET, barrier materials such as Phenoxy-type Thermoplastics, polyamides and Polyamide Blends, and other materials such as recycled PET may be used in combination with other materials which enhance or provide the barrier properties. Generally speaking, one cause for the diffusion of gases through a material is the existence of gaps or holes in the material at the molecular level through which the gas molecules can pass. The presence of intermolecular forces in a material, such as hydrogen bonding, allows for interchain cohesion in the matrix which closes these gaps and discourages diffusion of gases. One may also increase the gas-barrier ability of good barrier materials by adding an additional molecule or substance which takes advantage of such intermolecular forces and acts as a bridge between polymer chains in the matrix, thus helping to close the holes in the matrix and reduce gas diffusion.

Derivatives of the diol resorcinol (m-dihydroxybenzene), when reacted with other monomers in the manufacture of PHAE, PET, Copolyester Barrier Materials, and other barrier materials, will generally result in a

material which has better barrier properties than the same material if it does not contain the resorcinol derivative. For example, resorcinol diglycidyl ether can be used in PHAE and hydroxyethyl ether resorcinol can be used in PET and other polyesters and Copolyester Barrier Materials.

One measure of the efficacy of a barrier is the effect that it has upon the shelf life of the material. The shelf life of a carbonated soft drink in a 32 oz PET non-barrier bottle is approximately 12-16 weeks. Shelf life is determined as the time at which less than 85% of the original amount of carbon dioxide is remaining in the bottle. Bottles coated with PHAE using the inject-over-inject method described below have been found to have a shelf life 2 to 3 times greater than that of PET alone. If, however, PHAE with resorcinol diglycidyl ether is used, the shelf life can be increased to 4 to 5 times that of PET alone.

Another way of enhancing the barrier properties of a material is to add a substance which "plugs" the holes in the polymer matrix and thus discourages gases from passing through the matrix. Alternatively, a substance may aid in creating a more tortuous path for gas molecules to take as they permeate a material. One such substance, referred to herein by the term "Nanoparticles" or "nanoparticulate material" are tiny particles of materials which enhance the barrier properties of a material by creating a more tortuous path for migrating oxygen or carbon dioxide. One preferred type of nanoparticulate material is a microparticulate clay-based product available from Southern Clay Products.

Another way to provide or enhance barrier properties is to include an oxygen scavenger. Oxygen scavengers may be blended with a material by physical blending or mixing of the oxygen scavenger with pellets or flakes of a polymer or by compounding the oxygen scavenger with the polymer. Preferred oxygen scavengers include Amosorb 3000 from Amoco. Preferably, the oxygen scavenger is added at a level of 0.5 to 15% by weight, more preferably 1 to 10% by weight, including 5%, 7% and 9%. Other scavengers may be added at volumes which achieve the desired degree of effect, or at levels at or below which they have been approved for use in connection with packaging such as for foods.

#### **E. Preparing Barrier-Coated Articles**

Once a suitable barrier coating material is chosen, the coated preform must be made in a manner that promotes adhesion between the two materials. Generally, adherence between the barrier coating materials and PET increases as the surface temperature of the PET increases. Therefore, it is preferable to perform coating on heated preforms, although the preferred barrier materials will adhere to PET at room temperature. Although this discussion is in terms of barrier materials, the same principles noted herein apply to the coating or overmolding of RPET and PET and other such combinations of materials.

There are a number of methods of producing a coated PET preform in accordance with the preferred embodiments. Preferred methods include dip-coating, spray coating, flame spraying fluidized bed dipping, and electrostatic powder spraying. Each of the above methods is described in copending U.S. Application Serial No. 09/147,971, which was filed on October 19, 1998, entitled BARRIER-COATED POLYESTER, which is hereby incorporated by reference in its entirety.



An especially preferred method of producing a coated PET preform is referred to herein generally as overmolding, and sometimes as inject-over-inject ("IOI"). The name refers to a procedure which uses injection molding to inject one or more layers of barrier material over an existing preform, which preferably was itself made by injection molding. The terms "overinjecting" and "overmolding" are used herein to describe the coating process whereby a layer of material, preferably comprising barrier material, is injected over an existing preform. In an especially preferred embodiment, the overinjecting process is performed while the underlying preform has not yet fully cooled. Overinjecting may be used to place one or more additional layers of materials such as those comprising barrier material, recycled PET, or other materials over a coated or uncoated preform. The IOI process is described in the application noted above as well as copending U.S. Application Serial No. 09/296,695, which was filed on April 21, 1999 entitled **APPARATUS AND METHOD FOR MAKING BARRIER-COATED POLYESTER**, which is hereby incorporated by reference in its entirety.

**1. Preferred Overmolding (Inject-over-Inject) Processes**

The overmolding is preferably carried out by using an injection molding process using equipment similar to that used to form the uncoated preform itself. A preferred mold for overmolding, with an uncoated preform in place is shown in FIGURE 7. The mold comprises two halves, a cavity half 92 and a mandrel half 94, and is shown in FIGURE 7 in the closed position prior to overinjecting. The cavity half 92 comprises a cavity in which the uncoated preform is placed. The support ring 38 of the preform rests on a ledge 96 and is held in place by the mandrel half 94, which exerts pressure on the support ring 38, thus sealing the neck portion off from the body portion of the preform. The cavity half 92 has a plurality of tubes or channels 104 therein which carry a fluid. Preferably the fluid in the channels circulates in a path in which the fluid passes into an input in the cavity half 92, through the channels 104, out of the cavity half 92 through an output, through a chiller or other cooling device, and then back into the input. The circulating fluid serves to cool the mold, which in turn cools the plastic melt which is injected into the mold to form the coated preform.

The mandrel half 94 of the mold comprises a mandrel 98. The mandrel 98, sometimes called a core, protrudes from the mandrel half 94 of the mold and occupies the central cavity of the preform. In addition to helping to center the preform in the mold, the mandrel 98 cools the interior of the preform. The cooling is done by fluid circulating through channels 106 in the mandrel half 94 of the mold, most importantly through the length of the mandrel 98 itself. The channels 106 of the mandrel half 94 work in a manner similar to the channels 104 in the cavity half 92; in that they create the portion of the path through which the cooling fluid travels which lies in the interior of the mold half.

As the preform sits in the mold cavity, the body portion of the preform is centered within the cavity and is completely surrounded by a void space 100. The preform, thus positioned, acts as an interior die mandrel in the subsequent injection procedure. The melt of the overmolding material, preferably comprising a barrier material, is then introduced into the mold cavity from the injector via gate 102 and flows around the preform, preferably surrounding at

least the body portion 34 of the preform. Following overinjection, the overmolded layer will take the approximate size and shape of the void space 100.

To carry out the overmolding procedure, one preferably heats the initial preform which is to be coated preferably to a temperature above its  $T_g$ . In the case of PET, that temperature is preferably about 60 to 175°C, more preferably about 80-110°C. If a temperature at or above the minimum temperature of crystallization for PET is used, which is about 120°C, care should be taken when cooling the PET in the preform. The cooling should be sufficient to minimize crystallization of the PET in the preform so that the PET is in the preferred semi-crystalline state. Advantageously, the neck portion of the preform is not in contact with the melt of overriding material, and thus retains its crystalline structure. Alternatively, the initial preform used may be one which has been very recently injection molded and not fully cooled, as to be at an elevated temperature as is preferred for the overmolding process.

The coating material is heated to form a melt of a viscosity compatible with use in an injection molding apparatus. The temperature for this, the inject temperature, will differ among materials, as melting ranges in polymers and viscosities of melts may vary due to the history, chemical character, molecular weight, degree of branching and other characteristics of a material. For the preferred barrier materials disclosed above, the inject temperature is preferably in the range of about 160-325°C, more preferably 200 to 275°C. For example, for the Copolyester Barrier Material B-010, the preferred temperature is around 210°C, whereas for the PHAE XU-19040.00L, BLOX 0005 or BLOX 0003 the preferred temperature is in the range of 160-260°C, and is more preferably about 175-240°C. Most preferably, the PHAE inject temperature is about 175-200°C. If recycled PET is used, the inject temperature is preferably 250-320°C. The coating material is then injected into the mold in a volume sufficient to fill the void space 100. If the coating material comprises barrier material, the coating layer is a barrier layer.

The coated preform is preferably cooled at least to the point where it can be displaced from the mold or handled without being damaged, and removed from the mold where further cooling may take place. If PET is used, and the preform has been heated to a temperature near or above the temperature of crystallization for PET, the cooling should be fairly rapid and sufficient to ensure that the PET is primarily in the semi-crystalline state when the preform is fully cooled. As a result of this process, a strong and effective bonding takes place between the initial preform and the subsequently applied coating material.

Overmolding can be also used to create coated preforms with three or more layers. In FIGURE 14, there is shown a three-layer embodiment of a preform 132 in accordance with one preferred embodiment. The preform shown therein has two coating layers, a middle layer 134 and an outer layer 134. The relative thickness of the layers shown in Figure 16 may be varied to suit a particular combination of layer materials or to allow for the making of different sized bottles. As will be understood by one skilled in the art, a procedure analogous to that disclosed above would be followed, except that the initial preform would be one which had already been coated, as by one of the methods for making coated preforms described herein, including overmolding.

a. A Preferred Method and Apparatus for Overmolding

A preferred apparatus for performing the overmolding process is based upon the use of a 330-330-200 machine by Engel (Austria). The preferred mold portion the machine is shown schematically in FIGURES 8-13 and comprises a movable half 142 and a stationary half 144. Both halves are preferably made from hard metal. The stationary half 144 comprises at least two mold sections 146, 148, wherein each mold section comprises  $N$  ( $N > 0$ ) identical mold cavities 114, 120, an input and output for cooling fluid, channels allowing for circulation of cooling fluid within the mold section, injection apparatus, and hot runners channeling the molten material from the injection apparatus to the gate of each mold cavity. Because each mold section forms a distinct preform layer, and each preform layer is preferably made of a different material, each mold section is separately controlled to accommodate the potentially different conditions required for each material and layer. The injector associated with a particular mold section injects a molten material, at a temperature suitable for that particular material, through that mold section's hot runners and gates and into the mold cavities. The mold section's own input and output for cooling fluid allow for changing the temperature of the mold section to accommodate the characteristics of the particular material injected into a mold section. Consequently, each mold section may have a different injection temperature, mold temperature, pressure, injection volume, cooling fluid temperature, etc. to accommodate the material and operational requirements of a particular preform layer.

The movable half 142 of the mold comprises a turntable 130 and a plurality of cores or mandrels 98. The alignment pins guide the movable half 142 to slidably move in a preferably horizontal direction towards or away from the stationary half 144. The turntable 130 may rotate in either a clockwise or counterclockwise direction, and is mounted onto the movable half 142. The plurality of mandrels 98 are affixed onto the turntable 130. These mandrels 98 serve as the mold form for the interior of the preform, as well as serving as a carrier and cooling device for the preform during the molding operation. The cooling system in the mandrels is separate from the cooling system in the mold sections.

The mold temperature or cooling for the mold is controlled by circulating fluid. There is separate cooling fluid circulation for the movable half 142 and for the overmolding section 148 of the stationary half 144. Additionally, the initial preform mold section 146 of the stationary half 144 comprises two separate cooling fluid circulation systems; one for the non-crystalline regions and one for the crystalline regions. Each cooling fluid circulation set up works in a similar manner. The fluid enters the mold, flows through a network of channels or tubes inside as discussed above for FIGURE 7, and then exits through an output. From the output, the fluid travels through a pump, which keeps the fluid flowing, and a chilling system to keep the fluid within the desired temperature range, before going back into the mold.

In a preferred embodiment, the mandrels and cavities are constructed of a high heat transfer material, such as beryllium, which is coated with a hard metal, such as tin or chrome. The hard coating keeps the beryllium from direct contact with the preform, as well as acting as a release for ejection and providing a hard surface for long life. The high heat transfer material allows for more efficient cooling, and thus assists in achieving lower cycle times. The high heat transfer material may be disposed over the entire area of each mandrel and/or cavity, or it may be only on

portions thereof. Preferably at least the tips of the mandrels comprise high heat transfer material. Another, even more preferred high heat transfer material is AMPICOLOY, which is commercially available from Uudenholm, Inc.

The number of mandrels is equal to the total number of cavities, and the arrangement of the mandrels 98 on the movable half 142 mirrors the arrangement of the cavities 114, 120 on the stationary half 144. To close the mold, the movable half 142 moves towards the stationary half 144, mating the mandrels 98 with the cavities 114, 120. To open the mold, the movable half 142 moves away from the stationary half 144 such that the mandrels 98 are well clear of the block on the stationary half 144. After the mandrels are fully withdrawn 98 from the mold sections 146, 148, the turntable 130 of the movable half 142 rotates the mandrels 98 into alignment with a different mold section. Thus, the movable half rotates  $360^\circ/(\text{number of mold sections in the stationary half})$  degrees after each withdrawal of the mandrels from the stationary half. When the machine is in operation, during the withdrawal and rotation steps, there will be preforms present on some or all of the mandrels.

The size of the cavities in a given mold section 146, 148 will be identical; however the size of the cavities will differ among the mold sections. The cavities in which the uncoated preforms are first molded, the preform molding cavities 114, are smallest in size. The size of the cavities 120 in the mold section 148 in which the first coating step is performed are larger than the preform molding cavities 114, in order to accommodate the uncoated preform and still provide space for the coating material to be injected to form the overmolded coating. The cavities in each subsequent mold section wherein additional overmolding steps are performed will be increasingly larger in size to accommodate the preform as it gets larger with each coating step.

After a set of preforms has been molded and overmolded to completion, a series of ejectors eject the finished preforms off of the mandrels 98. The ejectors for the mandrels operate independently, or at least there is a single ejector for a set of mandrels equal in number and configuration to a single mold section, so that only the completed preforms are ejected. Uncoated or incompletely-coated preforms remain on the mandrels so that they may continue in the cycle to the next mold section. The ejection may cause the preforms to completely separate from the mandrels and fall into a bin or onto a conveyor. Alternatively, the preforms may remain on the mandrels after ejection, after which a robotic arm or other such apparatus grasps a preform or group of preforms for removal to a bin, conveyor, or other desired location.

FIGURES 8 and 9 illustrate a schematic for an embodiment of the apparatus described above. FIGURE 9 is the stationary half 144 of the mold. In this embodiment, the block 124 has two mold sections, one section 146 comprising a set of three preform molding cavities 114 and the other section 148 comprising a set of three preform coating cavities 120. Each of the preform coating cavities 120 is preferably like that shown in FIGURE 7, discussed above. Each of the preform molding cavities 114 is preferably similar to that shown in FIGURE 15, in that the material is injected into a space defined by the mandrel 98 (albeit without a preform already thereon) and the wall of the mold which is cooled by fluid circulating through channels inside the mold block. Consequently, one full production cycle of this apparatus will yield three two-layer preforms. If more than three preforms per cycle is desired, the stationary half can be reconfigured to accommodate more cavities in each of the mold sections. An example of this is seen in FIGURE

11; wherein there is shown a stationary half of a mold comprising two mold sections, one 146 comprising forty-eight preform molding cavities 114 and the other 148 comprising forty-eight preform coating cavities 120. If a three or more layer preform is desired, the stationary half 144 can be reconfigured to accommodate additional mold sections, one for each preform layer

5 FIGURE 8 illustrates the movable half 142 of the mold. The movable half comprises six identical mandrels 98 mounted on the turntable 130. Each mandrel 98 corresponds to a cavity on the stationary half 144 of the mold. The movable half also comprises alignment pegs 110, which correspond to the receptacles 112 on the stationary half 144. When the movable half 142 of the mold moves to close the mold, the alignment pegs 110 are mated with their corresponding receptacles 112 such that the molding cavities 114 and the coating cavities 120 align with the  
10 mandrels 98. After alignment and closure, half of the mandrels 98 are centered within preform molding cavities 114 and the other half of the mandrels 98 are centered within preform coating cavities 120.

The configuration of the cavities, mandrels, and alignment pegs and receptacles must all have sufficient symmetry such that after the mold is separated and rotated the proper number of degrees, all of the mandrels line up with cavities and all alignment pegs line up with receptacles. Moreover, each mandrel must be in a cavity in a different  
15 mold section than it was in prior to rotation in order to achieve the orderly process of molding and overmolding in an identical fashion for each preform made in the machine.

Two views of the two mold halves together are shown in FIGURES 12 and 13. In FIGURE 12, the movable half 142 is moving towards the stationary half 144, as indicated by the arrow. Two mandrels 98, mounted on the turntable 130, are beginning to enter cavities, one enters a molding cavity 114 and the other is entering a coating  
20 cavity 120 mounted in the block 124. In FIGURE 13, the mandrels 98 are fully withdrawn from the cavities on the stationary side. The preform molding cavity 114 has two cooling circulation systems which are separate from the cooling circulation for the preform coating cavity 120, which comprises the other mold section 148. The two mandrels 98 are cooled by a single system that links all the mandrels together. The arrow in FIGURE 13 shows the rotation of the turntable 130. The turntable 130 could also rotate clockwise. Not shown are coated and uncoated preforms  
25 which would be on the mandrels if the machine were in operation. The alignment pegs and receptacles have also been left out for the sake of clarity.

The operation of the overmolding apparatus will be discussed in terms of the preferred two mold section apparatus for making a two-layer preform. The mold is closed by moving the movable half 142 towards the stationary half 144 until they are in contact. A first injection apparatus injects a melt of first material into the first mold section  
30 146, through the hot runners and into the preform molding cavities 114 via their respective gates to form the uncoated preforms each of which become the inner layer of a coated preform. The first material fills the void between the preform molding cavities 114 and the mandrels 98. Simultaneously, a second injection apparatus injects a melt of second material into the second mold section 148 of the stationary half 144, through the hot runners and into each preform coating cavity 120 via their respective gates, such that the second material fills the void (100 in Figure 9)  
35 between the wall of the coating cavity 120 and the uncoated preform mounted on the mandrel 98 therein.

During this entire process, cooling fluid is circulating through the four separate areas, corresponding to the non-crystalline regions of mold section 146 of the preform molding cavities 114, the crystalline regions of mold section 146 of the preform molding cavities 114, mold section 148 of the preform coating cavities 120, and the movable half 142 of the mold, respectively. Thus, the melts and preforms are being cooled in the center by the circulation in the movable half that goes through the interior of the mandrels, as well as on the outside by the circulation in each of the cavities.

The movable half 142 then slides back to separate the two mold halves and open the mold until all of the mandrels 98 having preforms thereon are completely withdrawn from the preform molding cavities 114 and preform coating cavities 120. The ejectors eject the coated, finished preforms off of the mandrels 98 which were just removed from the preform coating cavities. As discussed above, the ejection may cause the preforms to completely separate from the mandrels and fall into a bin or onto a conveyor, or if the preforms remain on the mandrels after ejection, a robotic arm or other apparatus may grasp a preform or group of preforms for removal to a bin, conveyor, or other desired location. The turntable 130 then rotates 180° so that each mandrel 98 having an uncoated preform thereon is positioned over a preform coating cavity 120, and each mandrel from which a coated preform was just ejected is positioned over a preform molding cavity 114. Rotation of the turntable 130 may occur as quickly as 0.5-0.9 seconds. Using the alignment pegs 110, the mold halves again align and close, and the first injector injects the first material into the preform molding cavity 114 while the second injector injects the barrier material into the preform coating cavity 120.

A production cycle of closing the mold, injecting the melts, opening the mold, ejecting finished barrier preforms, rotating the turntable, and closing the mold is repeated, so that preforms are continuously being molded and overmolded.

When the apparatus first begins running, during the initial cycle, no preforms are yet in the preform coating cavities 120. Therefore, the operator should either prevent the second injector from injecting the second material into the second mold section during the first injection, or allow the second material to be injected and eject and then discard the resulting single layer preform comprised solely of the second material. After this start-up step, the operator may either manually control the operations or program the desired parameters such that the process is automatically controlled.

Two layer preforms may be made using the first preferred overmolding apparatus described above. In one preferred embodiment, the two layer preform comprises an inner layer comprising polyester and an outer layer comprising barrier material. In especially preferred embodiments, the inner layer comprises virgin PET. The description hereunder is directed toward the especially preferred embodiments of two layer preforms comprising an inner layer of virgin PET, in which the neck portion is generally crystalline and the body portion is generally non-crystalline. The description is directed toward describing the formation of a single set of coated preforms 60 of the type seen in FIGURE 4, that is, following a set of preforms through the process of molding, overmolding and ejection, rather than describing the operation of the apparatus as a whole. The process described is directed toward preforms having a

total thickness in the wall portion 66 of about 3 mm, comprising about 2 mm of virgin PET and about 1 mm of barrier material. The thickness of the two layers will vary in other portions of the preform 60, as shown in FIGURE 4.

It will be apparent to one skilled in the art that some of the parameters detailed below will differ if other embodiments of preforms are used. For example, the amount of time which the mold stays closed will vary depending upon the wall thickness of the preforms. However, given the disclosure below for this preferred embodiment and the remainder of the disclosure herein, one skilled in the art would be able to determine appropriate parameters for other preform embodiments.

The apparatus described above is set up so that the injector supplying the mold section 146 containing the preform molding cavities 114 is fed with virgin PET and that the injector supplying the mold section 148 containing the preform coating cavities 120 is fed with a barrier material.

The movable half 142 of the mold is moved so that the mold is closed. A melt of virgin PET is injected through the back of the block 124 and into each preform molding cavity 114 to form an uncoated preform 30 which becomes the inner layer of the coated preform. The injection temperature of the PET melt is preferably 250 to 320°C, more preferably 255 to 280°C. The mold is kept closed for preferably 3 to 10 seconds, more preferably 4 to 6 seconds while the PET melt stream is injected and then cooled by the coolant circulating in the mold.

In the first step, the PET substrate is injection molded by injecting molten PET into the cavities formed by the molds and cores in the mold stack. When the cavity is filled, the resin in the body portion will come into contact with cooling surfaces and the resin in the neck finish will come into contact with the heated thread mold. As the PET in the neck finish cools, it will begin to crystallize as a result of this contact with the relatively hot mold. Once in contact, the crystallization will start and continue at a rate determined by time and temperature. When the neck finish portion of the molds are kept above the minimum temperature of crystallization of the PET used, crystallization will begin on contact. Higher temperatures will increase the rate of crystallization and decrease the time required to reach the optimum level of crystallization while maintaining post mold dimensional stability of the neck finish of the preform. At the same time the resin in the neck finish portion is cooling into a crystallized state, the resin in the body portion or lower body portion of the preform will be in contact with the chilled portions of the mold and thus cooled into an amorphous or semi-crystalline state.

The movable half 142 of the mold is then moved so that the two halves of the mold are separated at or past the point where the newly molded preforms, which remain on the mandrels 98, are clear of the stationary side 144 of the mold. When the mandrels 98 are clear of the stationary side 144 of the mold, the turntable 130 then rotates 180° so that each mandrel 98 having a molded preform thereon is positioned over a preform coating cavity 120. Thus positioned, each of the other mandrels 98 which do not have molded preforms thereon, are each positioned over a preform molding cavity 114. The mold is again closed. Preferably the time between removal from the preform molding cavity 114 to insertion into the preform coating cavity 120 is 1 to 10 seconds, and more preferably 1 to 3 seconds.

When the molded preforms are first placed into preform coating cavities 120, the exterior surfaces of the body portions of the preforms are not in contact with a mold surface. Thus, the exterior skin of the body portion is

still softened and hot as described above because the contact cooling is only from the mandrel inside. The high temperature of the exterior surface of the uncoated preform (which forms the inner layer of the coated preform) aids in promoting adhesion between the PET and barrier layers in the finished barrier coated preform. It is postulated that the surfaces of the materials are more reactive when hot, and thus chemical interactions between the barrier material and the virgin PET will be enhanced by the high temperatures. Barrier material will coat and adhere to a preform with a cold surface, and thus the operation may be performed using a cold initial uncoated preform, but the adhesion is markedly better when the overmolding process is done at an elevated temperature, as occurs immediately following the molding of the uncoated preform. As discussed earlier, the neck portion of the preform has desirably crystallized from the separated, thermally isolated cooling fluid systems in the preform molding cavity. Since the coating operation does not place barrier material on the neck portion, its crystalline structure is substantially undisturbed.

A second injection operation then follows in which a melt of a barrier material is injected into each preform coating cavity 120 to coat the preforms. The temperature of the melt of barrier material is preferably 160 to 325°C. The exact temperature range for any individual barrier material is dependent upon the specific characteristics of that barrier material, but it is well within the abilities of one skilled in the art to determine a suitable range by routine experimentation given the disclosure herein. For example, if BLOX 0005 or BLOX 0003 is used, the temperature of the melt (inject temperature) is preferably 160 to 260°C, more preferably 200 to 240°C, and most preferably 175 to 200°C. If the Copolyester Barrier Material B-010 is used, the injection temperature is preferably 160 to 260°C, more preferably 190 to 250°C. During the same time that this set of preforms are being overmolded with barrier material in the preform coating cavities 120, another set of uncoated preforms is being molded in the preform molding cavities 114 as described above.

The two halves of the mold are again separated preferably 3 to 10 seconds, more preferably 4 to 6 seconds following the initiation of the injection step. The preforms which have just been barrier coated in the preform coating cavities 120, are ejected from the mandrels 98. The uncoated preforms which were just molded in preform molding cavities 114 remain on their mandrels 98. The turntable 130 is then rotated 180° so that each mandrel having an uncoated preform thereon is positioned over a coating cavity 120 and each mandrel 98 from which a coated preform was just removed is positioned over a molding cavity 114.

The cycle of closing the mold, injecting the materials, opening the mold, ejecting finished barrier preforms, rotating the turntable, and closing the mold is repeated, so that preforms are continuously being molded and overmolded. Those of skill in the art will appreciate that dry cycle time of the apparatus may increase the overall production cycle time for molding a complete preform.

The process using modified molds and chilled cores will produce a unique combination of amorphous/crystalline properties. As the core is chilled and the thread mold is heated, the thermal transfer properties of the PET act as a barrier to heat exchange. The heated thread molds crystallize the PET at the surface of the thread finish, and the PET material transitions into an amorphous form near the core as the temperature of the PET reduces



closer to the core. This variation of the material from the inner (core) portion to the outer (thread) portion is also referred to herein as the crystallinity gradient.

The core temperature and the rate of crystallization of the resin play a part in determining the depth of crystallized resin. In addition, the amorphous inner surface of the neck finish stabilizes the post mold dimensions allowing closer molding tolerances than other crystallizing processes. On the other side, the crystallized outer surface supports the amorphous structure during high temperature filling of the container. Physical properties are also enhanced (e.g. brittleness, impact etc.) as a result of this unique crystalline/amorphous structure.

The optimum temperature for crystallization may vary depending upon factors including resin grade, resin crystallization temperature, intrinsic viscosity, wall thickness, exposure time, mold temperature. Preferred resins include PET homopolymer and copolymers (including but not limited to high-IPA PET, Copolyester Barrier Materials, and copolymers of PET and polyamides) and PEN. Such resins preferably have low intrinsic viscosities and moderate melt temperatures, preferably IVs of about 74 to 86, and melt temperatures of about 220-300°C. The preferred mold temperature range for PET is from about 240-280°C, with the maximum crystallization rate occurring at about 180°C, depending upon the above factors, the preferred exposure time range is from about 20 to 60 seconds overall, which includes both injection steps in inject-over-inject embodiments, and the preferred injection cavity pressure range is about 5000 to 22000 PSI. Thicker finish wall thickness will require more time to achieve a particular degree of crystallinity as compared to that needed for a thinner wall thickness. Increases in exposure time (time in mold) will increase the depth of crystallinity and the overall percentage of crystallinity in the area, and changes in the mold temperature in the region for which crystallinity is desired will affect the crystallinity rate and dimensional stability.

One of the many advantages of using the process disclosed herein is that the cycle times for the process are similar to those for the standard process to produce uncoated preforms; that is the molding and coating of preforms by this process is done in a period of time similar to that required to make uncoated PET preforms of similar size by standard methods currently used in preform production. Therefore, one can make barrier coated PET preforms instead of uncoated PET preforms without a significant change in production output and capacity.

If a PET melt cools slowly, the PET will take on a crystalline form. Because crystalline polymers do not blow mold as well as amorphous polymers, a preform comprised of a body portion of crystalline PET would not be expected to perform as well in forming containers as one having a body portion formed of PET having a generally non-crystalline form. If, however, the body portion is cooled at a rate faster than the crystal formation rate, as is described herein, crystallization of the PET will be minimized and the PET will take on an amorphous or semi-crystalline form. Thus, sufficient cooling of the PET in the body portion of the preform is crucial to forming preforms which will perform as needed when processed.

The rate at which a layer of PET cools in a mold such as described herein is proportional to the thickness of the layer of PET, as well as the temperature of the cooling surfaces with which it is in contact. If the mold temperature factor is held constant, a thick layer of PET cools more slowly than a thin layer. This is because it takes a longer period of time for heat to transfer from the inner portion of a thick PET layer to the outer surface of the PET

which is in contact with the cooling surfaces of the mold than it would for a thinner layer of PET because of the greater distance the heat must travel in the thicker layer. Thus, a preform having a thicker layer of PET needs to be in contact with the cooling surfaces of the mold for a longer time than does a preform having a thinner layer of PET. In other words, with all things being equal, it takes longer to mold a preform having a thick wall of PET than it takes to mold a preform having a thin wall of PET.

The uncoated preforms, including those made by the first injection in the above-described apparatus, are preferably thinner than a conventional PET preform for a given container size. This is because in making the barrier coated preforms, a quantity of the PET which would be in a conventional PET preform can be displaced by a similar quantity of one of the preferred barrier materials. This can be done because the preferred barrier materials have physical properties similar to PET, as described above. Thus, when the barrier materials displace an approximately equal quantity of PET in the walls of a preform or container, there will not be a significant difference in the physical performance of the container. Because the preferred uncoated preforms which form the inner layer of the barrier coated preforms are thin-walled, they can be removed from the mold sooner than their thicker-walled conventional counterparts. For example, the uncoated preform can be removed from the mold preferably after about 4-6 seconds without the body portion crystallizing, as compared to about 12-24 seconds for a conventional PET preform having a total wall thickness of about 3 mm. All in all, the time to make a barrier coated preform is equal to or slightly greater (up to about 30%) than the time required to make a monolayer PET preform of this same total thickness.

Additionally, because the preferred barrier materials are amorphous, they will not require the same type of treatment as the PET. Thus, the cycle time for a molding-overmolding process as described above is generally dictated by the cooling time required by the PET. In the above-described method, barrier coated preforms can be made in about the same time it takes to produce an uncoated conventional preform.

The advantage gained by a thinner preform can be taken a step farther if a preform made in the process is of the type in FIGURE 4. In this embodiment of a coated preform, the PET wall thickness at 70 in the center of the area of the end cap 42 is reduced to preferably about 1/3 of the total wall thickness. Moving from the center of the end cap out to the end of the radius of the end cap, the thickness gradually increases to preferably about 2/3 of the total wall thickness, as at reference number 68 in the wall portion 66. The wall thickness may remain constant or it may, as depicted in FIGURE 4, transition to a lower thickness prior to the support ring 38. The thickness of the various portions of the preform may be varied, but in all cases, the PET and barrier layer wall thicknesses must remain above critical melt flow thickness for any given preform design.

Using preforms 60 of the design in FIGURE 4 allows for even faster cycle times than that used to produce preforms 50 of the type in FIGURE 3. As mentioned above, one of the biggest barriers to short cycle time is the length of time that the PET needs to be cooled in the mold following injection. If the body portion of a preform comprising PET has not sufficiently cooled before it is ejected from the mandrel, it will become substantially crystalline and potentially cause difficulties during blow molding. Furthermore, if the PET layer has not cooled enough before the overmolding process takes place, the force of the barrier material entering the mold will wash away some of the PET

near the gate area. The preform design in FIGURE 4 takes care of both problems by making the PET layer thinnest in the center of the end cap region 42, which is where the gate is in the mold. The thin gate section allows the gate area to cool more rapidly, so that the uncoated PET layer may be removed from the mold in a relatively short period of time while still avoiding crystallization of the gate area and washing of the PET during the second injection or overmolding phase.

The physical characteristics of the preferred barrier materials help to make this type of preform design workable. Because of the similarity in physical properties, containers having wall portions which are primarily barrier material can be made without sacrificing the performance of the container. If the barrier material used were not similar to PET, a container having a variable wall composition as in FIGURE 4 would likely have weak spots or other defects that could affect container performance.

#### b. Improving Mold Performance

As discussed above, the mold halves have an extensive cooling system comprising circulating coolant throughout the mold in order to conduct heat away and thus enhance the mold's heat absorption properties. With next reference to FIGURE 15, which is a cross-section of a mold mandrel 298 and cavity 300 having features in accordance with preferred embodiments, the mold cooling system can be optimized for the mold cavities by arranging cooling tubes 302 in a spiral around the mold cavity 300 and just below the surface 304. The rapid cooling enabled by such a cooling system helps avoid crystallization of the PET layer in the body portion of the preform during cooling. Also, the rapid cooling decreases the production cycle time by allowing injected preforms to be removed from the mold cavities quickly so that the mold cavity 300 may be promptly reused.

As discussed above, the gate area 306 of the mold cavity 300 is especially pivotal in determining cycle time. The void space near the gate 308, which will make up the molded preform's base end 304, receives the last portion of the melt stream to be injected into the mold cavity 300. Thus, this portion is the last to begin cooling. If the PET layer has not sufficiently cooled before the overmolding process takes place, the force of the barrier material melt entering the mold may wash away some of the PET near the gate area 308. To speed cooling in the gate area of the mold cavity in order to decrease cycle time, inserts 310 of an especially high heat transfer material, including, but not limited to, a beryllium-free copper alloy (sold under the trade name AMPCOLOY), can be disposed in the mold in the gate area 308. These AMPCOLOY inserts 310 will withdraw heat at an especially fast rate. To enhance and protect the AMPCOLOY inserts 310, a thin layer of titanium nitride or hard chrome may be deposited on the surface 312 of the AMPCOLOY to form a hard surface. Such a deposited surface would be preferably between only 0.001 to 0.01 inches thick and would most preferably be about 0.002 inches thick.

As discussed above, the mandrel 298 is especially important in the cooling process because it directly cools the inner PET layer. To enhance the cooling effect of the mandrel 298 on the inner surface of the preform and especially to enhance the cooling effect of the mandrel 298 at the preform's gate area/base end 314, the mandrel 298 is preferably substantially hollow, having a relatively thin uniform wall 320, as shown in Figure 26. Preferably, this uniform thickness is between 0.1 inch and 0.3 inches and is most preferably about 0.2 inches. It is particularly

important that the wall 320 at the base end 322 of the mandrel 298 is no thicker than the rest of the mandrel wall 314 because the thin wall aids in rapidly communicating heat away from the molten gate area 314 of the injected preform.

To further enhance the mandrel's cooling capability, cooling water may be supplied in a bubbler arrangement 330. A core tube 332 is disposed centrally in the mandrel 298 and delivers chilled coolant C to the base end 322 thereof. Since the base end 322 is the first point of the mandrel 298 contacted by this coolant C, the coolant is coldest and most effective at this location. Thus, the gate area 314 of the injected preform is cooled at a faster rate than the rest of the preform. Coolant injected into the mandrel at the base end 322 proceeds along the length of the mandrel 298 and exits through an output line 334. A plurality of ribs 336 are arranged in a spiral pattern around the core tube 332 to direct coolant C along the mandrel wall.

In other embodiments where greater crystallinity and less crystalline gradient is desired, molds which are modified as described above are paired with cores modified as follows. In the modified cores, the fluid circulation in the cores is modified such that, for the portions to form the crystalline preform parts, the fluid circulation is independent and at a relatively higher temperature, or the flow of chilled fluid is restricted or altered in these regions such that the temperature of the surface of the core in the portion which forms the crystalline portion of the preform is higher than that in the body regions. Alternatively, the relevant portions of the core may be heated other means as described above. Use of cores having these characteristics allows for a greater degree of crystallization towards and/or at the inner surface of the preform in the neck, neck finish and/or neck cylinder area and a lesser crystalline gradient between the inner surface and the outer surface in these areas.

FIGURE 18 is a schematic representation of one such modified core 298', configured to achieve greater crystallinity of the neck portion of an injected preform. The mold of FIGURE 18 is similar in construction to the mold described above with reference to FIGURE 15. Accordingly, like reference characters will be used to describe like components, except that a (') will be used to denote modified components.

The core 298' of FIGURE 18 includes a double wall portion 408 generally adjacent to the neck finish portion 402 of the mold. An inner wall 410 substantially inhibits circulating fluid C from coming into contact with the outer wall 412 of the core 298' in the region proximate the neck finish portion 402 of the mold. In addition, an insulating space 414 is defined between the inner wall and outer wall 412. Accordingly, the insulating space 414 reduces the cooling effect of the circulating fluid C on the neck portion of a preform within the mold cavity 300 thereby increasing the crystallinity of the resulting preform, and reducing the crystallinity gradient between the outer surface and the inner surface of the resulting preform.

The inner wall 410 of the modified core 298 may optionally include one or more openings 416. These openings 416 permit circulating fluid C to enter the insulating space 414. Preferably, the size of the openings 416 are configured such that a limited amount of circulating fluid C enters the insulating space 414. Such a construction provides a greater cooling effect on the neck portion of the resulting preform than when no fluid is permitted within the insulating space 414, but less cooling than unrestricted contact of the circulating fluid C with the outer wall 412 of

the core 298. Advantageously, adjustment of the size and placement of the openings 416 allows adjustment of the cooling on the neck portion of the injected preform, thereby allowing adjustment of the crystallinity and crystallinity gradient in the neck portion.

FIGURE 19 is a schematic representation of another embodiment of a mandrel, or core 298'', including a modified base end 322 or tip. The mold core 298'' of FIGURE 19 is similar in construction to the mold described above with reference to FIGURE 15. Accordingly, like reference characters will be used to describe like components, except that a (') will be used to denote modified components.

As described above, the end cap portion of the injection molded preform adjacent the base end 322, receives the last portion of the melt stream to be injected into the mold cavity 300. Thus, this portion is the last to begin cooling. If the PET layer has not sufficiently cooled before the overmolding process takes place, the force of the barrier material melt entering the mold may wash away some of the PET near the base end 322 of the core 298. To speed cooling in the base end 322 of the core 298 in order to decrease cycle time, the modified core 298'' includes a base end 322'' portion constructed of an especially high heat transfer material, preferably a beryllium-free copper alloy, such as AMPCOLOY. Advantageously, the AMPCOLOY base end 322'' allows the circulating fluid C to withdraw heat from the injected preform at a higher rate than the remainder of the core 298''. Such a construction allows the end cap portion of the preform to cool quickly, in order to decrease the necessary cooling time and, thus, reduce the cycle time of the initial preform injection.

The modified core 298'' illustrated in FIGURE 19 generally comprises an upper core portion 418, substantially as illustrated in FIGURE 15, and a base end portion 322'' constructed of a high heat transfer material, including, but not limited to, a beryllium-free copper alloy, such as AMPCOLOY. A core tube 332, substantially as described above, is illustrated in phantom. As in FIGURE 15, the present core tube 332 is operable for delivering circulating cooling fluid to the base end 322'' of the core 298''.

The core 298'' is substantially hollow and defines an inner diameter D and wall thickness T. The upper core portion 418 includes a recessed step 420 having a diameter  $D_s$  which is greater than the inner diameter D of the core 298''. The base end portion 322'' includes a flange 422 having a diameter  $D_f$  which is smaller than the diameter  $D_s$  of the step 420. The difference between the diameters  $D_s$  and  $D_f$  of the step 420 and flange 422, respectively, is preferably between 0.000 and 0.025 inches. More preferably, the difference is between 0.010 and 0.015 inches. When the base end portion 322'' is placed concentrically within the upper core portion 418, the difference in the diameters  $D_s$ ,  $D_f$  results in a gap G being formed between the base end and upper core portions 322'', 418. The width W of the gap G is approximately equal to one-half the difference between the diameters  $D_s$ ,  $D_f$ . Additionally, the base end portion 322'' is preferably about 0.750-1.250 inches in length.

Preferably, the modified core 298'' is constructed by starting with an unmodified core 298 made from a single material, substantially as illustrated in FIGURE 15. The end portion, or tip, of the unmodified core 298 is cut off approximately at the point where the high heat transfer base end 322'' is desired to begin. A drilling, or boring, tool may then be inserted from the end portion of the core 298'' to ensure that the inner diameter D is correctly sized and

concentric with a center axis of the core 298". This also ensures that the wall thickness T is consistent throughout the portion of the core 298" which is in contact with the injected preform, thus ensuring that the cooling of the preform is consistent as well. Such a method of construction presents a distinct advantage over conventionally formed cores. In a conventional core, because the length to diameter ratio is large, the drilling tool used to create the hollow inner portion of the core often tends to wander, that is, tends to deflect from the center axis of the core. The wandering of the drilling tool results in a core having an inconsistent wall thickness and, thus, inconsistent heat transfer properties. With the above-described method of sizing the inner diameter D from the base end of the core 298", the problem of tool wandering is substantially reduced or eliminated. Therefore, a consistent wall thickness T and, as a result, consistent heat transfer properties are achieved.

The upper core portion 418 and base end portion 322" are preferably joined by a silver solder process. AMPICOLOY is a preferred material for the base end portion 322" in part because it contains some silver. This allows the silver solder process to provide a joint of sufficient strength to be useful in injection molding applications. Preferably, the soldering process results in a full contact joint. That is, solder material is disposed on all of the mating surfaces (424, 426 and gap G) between the upper core portion 418 and base end portion 322". Advantageously, the provision of the gap G enhances the flow of solder material such that a strong joint is achieved. In addition, the full contact joint is advantageous because it provides for consistent heat transfer properties and high strength. If the soldered joint was not a full contact joint, any air present in the gap G would result in inconsistent heat transfer through the gap G portion of the core 298". Although it is preferred to join the upper core portion 418 and base end portion 322" with a silver solder process, other suitable joining processes may also be used.

As illustrated in FIGURE 19, the base end portion 322" of the modified core 298" is preferably of a larger size than the final dimension desired (illustrated by the dashed line 428) when it is joined to the upper core portion 418. Advantageously, this allows for the base end portion 322" to be machined to its desired dimension after assembly to the upper core portion 418 in order to ensure a proper final diameter and a smooth surface at the transfer from the upper core portion 418 to the base end portion 322".

Another way to enhance cooling of the preform's gate area was discussed above and involves forming the mold cavity so that the inner PET layer is thinner at the gate area than at the rest of the injected preform as shown in FIGURE 4. The thin gate area thus cools quickly to a substantially solid state and can be quickly removed from the first mold cavity, inserted into the second mold cavity, and have a layer of barrier material injected thereover without causing washing of the PET.

In the continuing effort to reduce cycle time, injected preforms are removed from mold cavities as quickly as possible. However, it may be appreciated that the newly injected material is not necessarily fully solidified when the injected preform is removed from the mold cavity. This results in possible problems removing the preform from the cavity 300. Friction or even a vacuum between the hot, malleable plastic and the mold cavity surface 304 can cause resistance resulting in damage to the injected preform when an attempt is made to remove it from the mold cavity

Typically, mold surfaces are polished and extremely smooth in order to obtain a smooth surface of the injected part. However, polished surfaces tend to create surface tension along those surfaces. This surface tension may create friction between the mold and the injected preform which may result in possible damage to the injected preform during removal from the mold. To reduce surface tension, the mold surfaces are preferably treated with a very fine sanding device to slightly roughen the surface of the mold. Preferably the sandpaper has a grit rating between about 400 and 700. More preferably a 600 grit sandpaper is used. Also, the mold is preferably sanded in only a longitudinal direction, further facilitating removal of the injected preform from the mold.

During injection, air is pushed out of the mold cavity 300 by the injected meltstream. As a result, a vacuum may develop between the injected preform and the mold cavity wall 304. When the injected preform is removed from the cavity 300, the vacuum may resist removal, resulting in damage to the not-fully-solidified preform. To defeat the vacuum, an air insertion system 340 may be employed. With additional reference to FIGURES 16 and 17, an embodiment of an air insertion system 340 is provided. At a joint 342 of separate members of the mold cavity 300, a notch 344 is preferably formed circumferentially around and opening into the mold cavity 300. The notch 344 is preferably formed by a step 346 of between 0.002 inches and 0.005 inches and most preferably about 0.003 inches in depth. Because of its small size, the notch 344 will not fill with plastic during injection but will enable air A to be introduced into the mold cavity 300 to overcome the vacuum during removal of the injected preform from the mold cavity 300. An air line 350 connects the notch 344 to a source of air pressure and a valve (not shown) controls the supply of air A. During injection, the valve is closed so that the melt fills the mold cavity 300 without air resistance. When injection is complete, the valve opens and a supply of air is delivered to the notch 344 at a pressure between about 75 psi and 150 psi and most preferably about 100 psi. The supply of air defeats any vacuum that may form between the injected preform and the mold cavity, aiding removal of the preform. Although the drawings show only a single air supply notch 344 in the mold cavity 300, any number of such notches may be provided and in a variety of shapes depending on the size and shape of the mold.

While some of the above-described improvements to mold performance are specific to the method and apparatus described herein, those of skill in the art will appreciate that these improvements may also be applied in many different types of plastic injection molding applications and associated apparatus. For instance, use of AMPCOLOY in a mold may quicken heat removal and dramatically decrease cycle times for a variety of mold types and melt materials. Also, roughening of the molding surfaces and provides air pressure supply systems may ease part removal for a variety of mold types and melt materials.

## 2. Preferred Dip Coating Processes

One preferred method of producing a coated preform in accordance with preferred embodiments is to dip coat the preform in a resin-containing solvent bath. The dipping of the preforms into the resin-containing bath can be done manually by the use of a retaining rack or the like, or it may be done by a fully automated process which may include the blow-molding process at the end.

The bath contains a solution made from one or more solvents into which the resin of the barrier material is dissolved and/or suspended. The term "solution" as used herein refers to end result of mixing solvent(s) and resin, whether the resulting combination is in solution, suspension, or some combination thereof. The resin may be used in any form, but as with most all materials, smaller sized particles go into solution faster than larger ones. If the barrier material is not very soluble in a given solvent, adding the resin as a powder will help create a more uniform suspension. A wide variety of solvents may be used, as well as solvent systems made of combinations of solvents. Preferred solvents include dimethylformamide (DMF), ethanol, tetrahydrofuran (THF), methylene chloride, water, acetone, benzene, toluene, Dowanol DPM, Dowanol PPH, and Dowanol PM, and mixtures thereof. Factors which influence the selection of solvent or solvent system include polarity, reactivity, solubility, boiling point, vapor pressure, and flammability. The dip-coating solutions of the present invention preferably contain 10-60% resin by weight, more preferably 20-50% resin by weight, most preferably 30-40% resin by weight. The temperature of the solution in the bath is preferably 0 to 100°C, more preferably 25 to 50°C. For PHAE materials, such as BLOX 0005, the solutions or dispersions used for dipping the preforms may be acidified solutions including those described in U.S. Patent No. 6,180,715, which is hereby incorporated by reference in its entirety.

The surface of the preform to be dipped is preferably free of any oils, surfactants, mold release agents, or the like so that the barrier coating material can adhere directly to the outer surface thereof. The preforms are then dipped into the solution in the bath. The preform is preferably dipped until at least the entire body portion 4 of the preform is submerged in the bath up to just under the support ring 6. The preform remains submerged in the bath preferably for 1 to 30 seconds, more preferably 2 to 5 seconds. The preform is then withdrawn from the bath and dried until no solvent remains on the preform. Drying may be done by any one of a number of methods, such as air-drying or placing the preforms under a vacuum and/or in a heated atmosphere as in an oven. The choice of method may depend upon the solvent chosen and the speed at which one desires the drying to take place. Additional dipping and drying steps may be done to create additional layers if desired. Preferably, further processing such as blow molding is done after the preform is dry.

Although the discussion above is in terms of preforms, the dipping process may also be done on bottles. The thickness of the barrier coating on the bottle or preform is preferably 0.01 to 3 mm, more preferably 0.1 to 1 mm.

In an exemplary process, a sample of a Phenoxy-type Thermoplastic resin, specifically a PHAE available from Dow Chemical Company as XU19040.001 was obtained as small pellets. The pellets were dissolved in dimethylformamide to a concentration of 40% by weight. Eight identical 17.5 g virgin PET preforms of the type used to make a 16 oz. carbonated beverage bottle were placed in a rack and dipped into the bath containing the resin/DMF solution which was at room temperature (approximately 21-23°C). After 5 seconds the preforms were removed from the bath and dried for 8 hours in an oven set at about 75°C.

Before dip-coating, the preforms weighed an average of 17.5 grams. After dip-coating the preforms weighted an average of 18.0 grams, having had 0.5 grams of resin coated thereon by the process.



### 3. Preferred Spray Coating Processes

Another method of producing coated articles, or providing additional coating layers, is by spray coating. In this method, the preforms or containers are sprayed with a solution of resin dissolved or suspended in a solvent. The spraying of the articles can be done manually or by use of an apparatus which provides for spraying and perhaps also post-spray treatment in one machine.

The solution or dispersion which is sprayed onto the articles contains one or more solvents into which the resin of the barrier material is dissolved and/or suspended. The solutions and dispersions mentioned above in reference to dip coating are preferably also used for spray coating. The solutions preferably contain 5 to 50% resin by weight, more preferably 30-40% resin by weight.

One preferred method of spray coating articles is based on the use of an apparatus such as that disclosed in U.S. Patent No. 4,538,542 to Kennon, et al. (incorporated herein in its entirety by this reference) and sold by Nordson Corporation (Amherst, Ohio). This apparatus comprises a spray coating chamber, a drying chamber, and a conveyor for moving the preforms between the two chambers. The apparatus may further comprise an overspray recovery system.

During a preferred spray coating process, the neck portion of each article is clasped by an attachment means and mounted on a conveyor. The articles are evenly spaced apart on the conveyor. The articles are thus conveyed into the spray coating chamber wherein they pass in close proximity to a series of spray nozzles, preferably airless spray nozzles. The resin-containing solvent is sprayed through the nozzles so that it impacts the outside surface of each article as it passes through the chamber, leaving each article covered with a wet coating layer. To aid the adherence of the sprayed material and help hasten the evaporation of the solvent, the articles may be pre-heated by use of radiant heaters or other methods known to those skilled in the art before they enter the spray coating chamber.

The conveyor then carries the articles out of the spray coating chamber and into the drying chamber. The drying chamber may comprise an oven, a collection of lamps, or other source of thermal energy which provides the chamber with a temperature warm enough to aid in driving off the solvent in the wet coating layer, yet not so hot as to cause distortion in the shape of the article itself. As the articles pass through the drying chamber, the solvent is evaporated, leaving a coating on the articles.

### F. Formation of Preferred Containers by Blow Molding

The coated containers preferably produced by blow-molding the coated preforms, the creation of which is disclosed above. The coated preforms can be blow-molded using techniques and conditions very similar to those by which uncoated PET preforms are blown into containers. In other preferred embodiments in which it is desired for the entire container to be heat-set, it is preferred that the containers be blow-molded in accordance with processes generally known for heat set blow-molding, including, but not limited to, those which involve orienting and heating in the mold, and those which involve steps of blowing, relaxing and reblowing.

For example, for preforms in which the neck finish is formed primarily of PET, the preform is heated to a temperature of preferably 80 to 120°C, with higher temperatures being preferred for the heat-set embodiments, and given a brief period of time to equilibrate. After equilibration, it is stretched to a length approximating the length of the

final container. Following the stretching, pressurized air is forced into the preform which acts to expand the walls of the preform to fit the mold in which it rests, thus creating the container.

Although the present invention has been described herein in terms of certain preferred embodiments, and certain exemplary methods, it is to be understood that the scope of the invention is not to be limited thereby. Instead,

- 5 Applicant intends that the scope of the invention be limited solely by reference to the attached claims, and that variations on the methods and materials disclosed herein which are apparent to those of skill in the art will fall within the scope of Applicant's invention.

WHAT IS CLAIMED IS:

1. An article comprising:  
a neck portion, and a body portion; wherein  
the neck portion and body portion are a monolithic first layer of material;  
5 the neck portion is primarily crystalline; and  
the body portion is primarily amorphous or semi-crystalline.
2. An article according to Claim 1, wherein the neck portion is threaded.
3. An article according to Claim 1, wherein the material is selected from the group consisting of PET  
homopolymers and copolymers, polyethylene naphthalate, polyethylene naphthalate copolymers, polyethylene  
10 naphthalate/polyethylene terephthalate blends, polyethylene terephthalate with PMDA, and combinations thereof.
4. An article according to Claim 1, the body portion additionally comprising a wall portion defining a  
first thickness, and an end cap defining a second thickness, the first thickness being greater than the second  
thickness.
5. An article according to Claim 1, wherein the body portion further comprises a second layer of  
15 material.
6. An article according to Claim 5, wherein at least one of the first and second layers of material have  
barrier properties.
7. An article according to Claim 5, wherein the second layer of material is a barrier material selected  
from the group consisting of Copolyester Barrier Materials, Phenoxy-type Thermoplastics, polyamides, Polyamide  
20 Blends, polyethylene naphthalate, polyethylene naphthalate copolymers, polyethylene naphthalate/polyethylene  
terephthalate blends, and combinations thereof.
8. An article according to Claim 5, wherein the second layer of material is recycled or post-consumer  
PET.
9. An article according to Claim 5, wherein the first layer of material comprises polyester and an  
25 oxygen scavenger and the second layer comprises recycled or post-consumer PET.
10. An article according to Claim 5, further comprising a third layer of material disposed over the  
second layer of material.
11. An article according to Claim 1, wherein a threaded neck finish thickness is defined from an  
exterior surface of the threaded neck finish to an interior surface of the threaded neck finish, the crystallinity being  
30 greater at the exterior surface than at the interior surface.
12. An article according to Claim 1, wherein the interior surface of the threaded neck finish is  
amorphous or semi-crystalline.
13. An article according to Claim 1, wherein the article is selected from the group consisting of bottles,  
preforms and containers.
- 35 14. A method of making a preform, comprising:

injecting a melt of a first material into a cavity formed by a mold and a core wherein the mold comprises a neck finish portion at a first temperature and a body portion at a second temperature, wherein the first temperature is greater than the crystallinity temperature of the first material and the second temperature is less than the crystallinity temperature of the first material;

5           leaving the melt of the first material in contact with the mold and core to form a preform wherein the body portion is primarily amorphous or semi-crystalline, and the neck finish is primarily crystalline; and removing the preform from the mold.

15           A method as in Claim 14, further comprising dipping or spraying at least the body portion of the preform with a solution or dispersion of a  
10           second material to form a two-layer preform.

16           A method as in Claim 14, further comprising placing the preform in a second mold wherein the second mold comprises a body portion at a third temperature;

15           injecting a second layer of polymer melt over the body portion to form a two-layer preform; and removing the two-layer preform from the mold.

17           A method as in Claim 16, further comprising dipping or spraying at least the body portion of the two-layer preform in a solution or dispersion of a third material to form a three-layer preform, wherein the third material is the same or different material from the first and second materials.

20           18. A method as in Claim 17, wherein the third material comprises PHAE.

19           A method as in Claim 16, further comprising blow-molding the preform to form a container or  
bottle.

20           20. A mold for making a preform, comprising:  
a neck finish portion having a first mold temperature control system;  
25           a body portion having a second temperature control system; and  
a core having a third temperature control system;  
wherein the first temperature control system is independent of the second and third temperature control systems and the neck finish portion is thermally isolated from the body portion and core.

21           A mold according to Claim 20, wherein the first, second and third temperature control systems  
30           comprise circulating fluid.

22           A mold according to Claim 20, wherein the first and second temperature control systems comprise components independently selected from the group consisting of heaters, heating coils, heating probes, and circulating fluid.

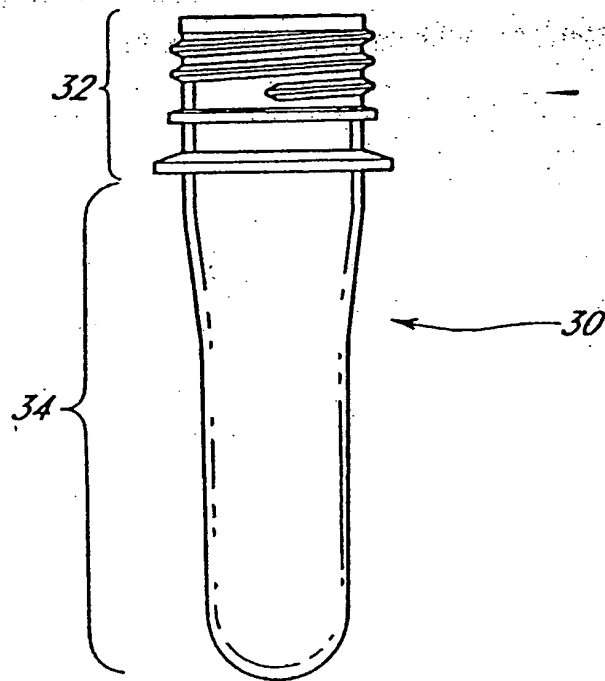
23. A mold according to Claim 20, wherein the core comprises a first core portion in the region of the threaded neck portion of the mold and a second core portion in the region of the body portion of the mold, wherein the first and second core portions have separate temperature regulation systems.

24. A mold according to Claim 23, wherein the first and second core temperature regulation systems are selected from the group consisting of heaters, heating coils, heating probes, and circulating fluid.

25. A mold according to Claim 20, wherein the core has a base end, the core additionally comprising a core tube extending toward the base end of the core, the third temperature control system comprising circulating fluid, the fluid being introduced through the core tube to the base end of the core.

26. A mold according to Claim 20, wherein the base end of the core is constructed from a material having a higher rate of heat transfer than an upper portion of the core.

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**FIG. 1**

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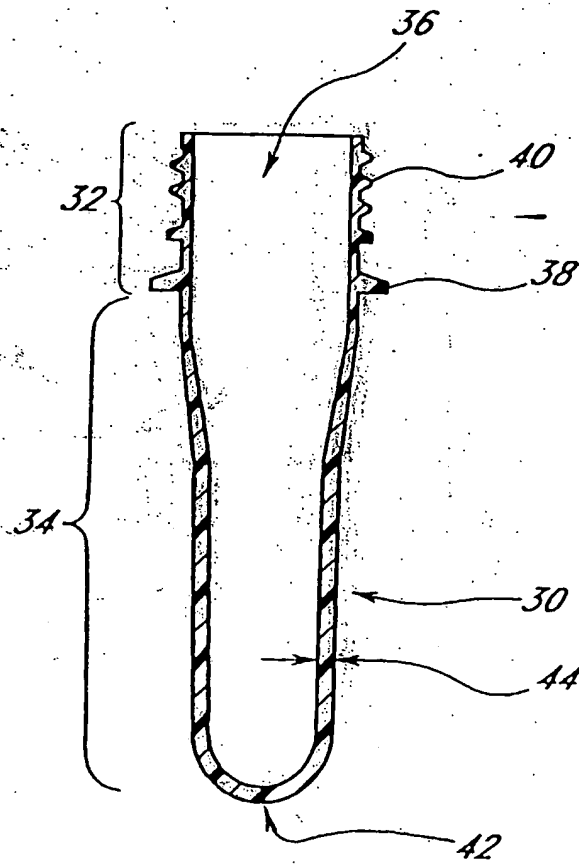


FIG. 2





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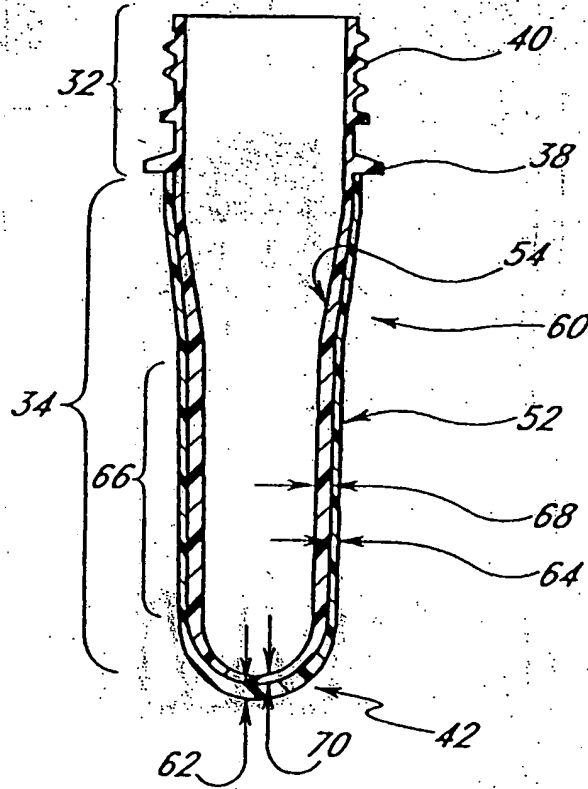


FIG. 4

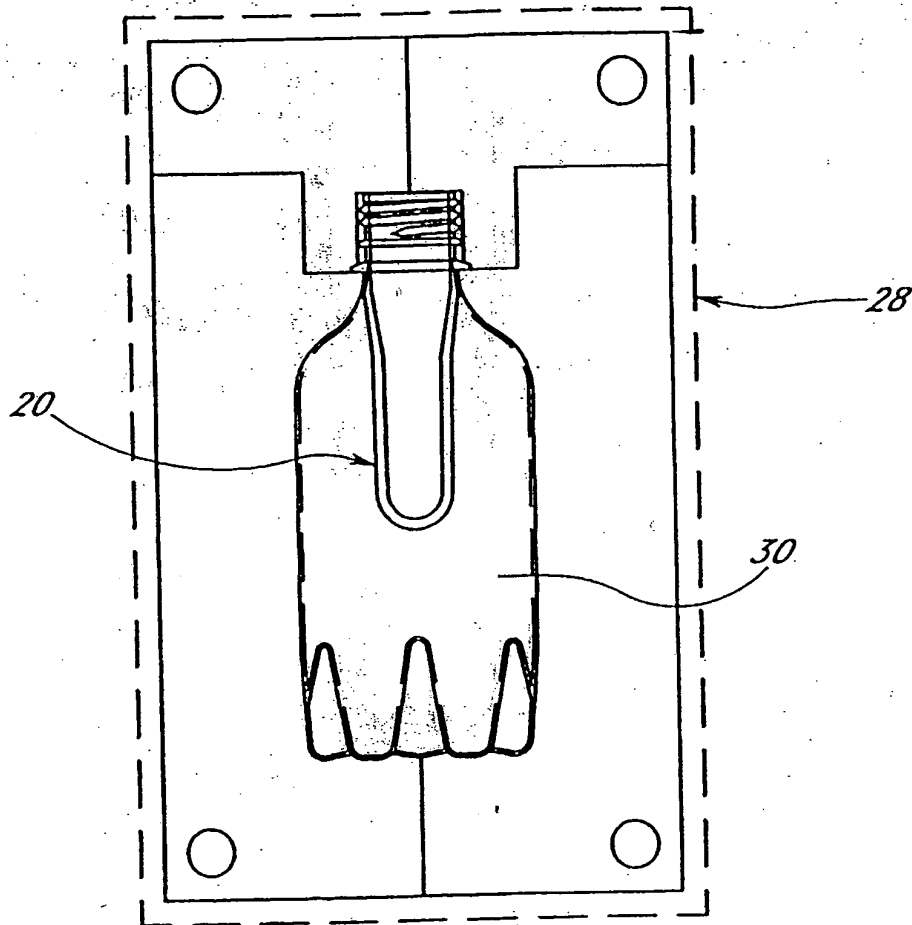


FIG. 5

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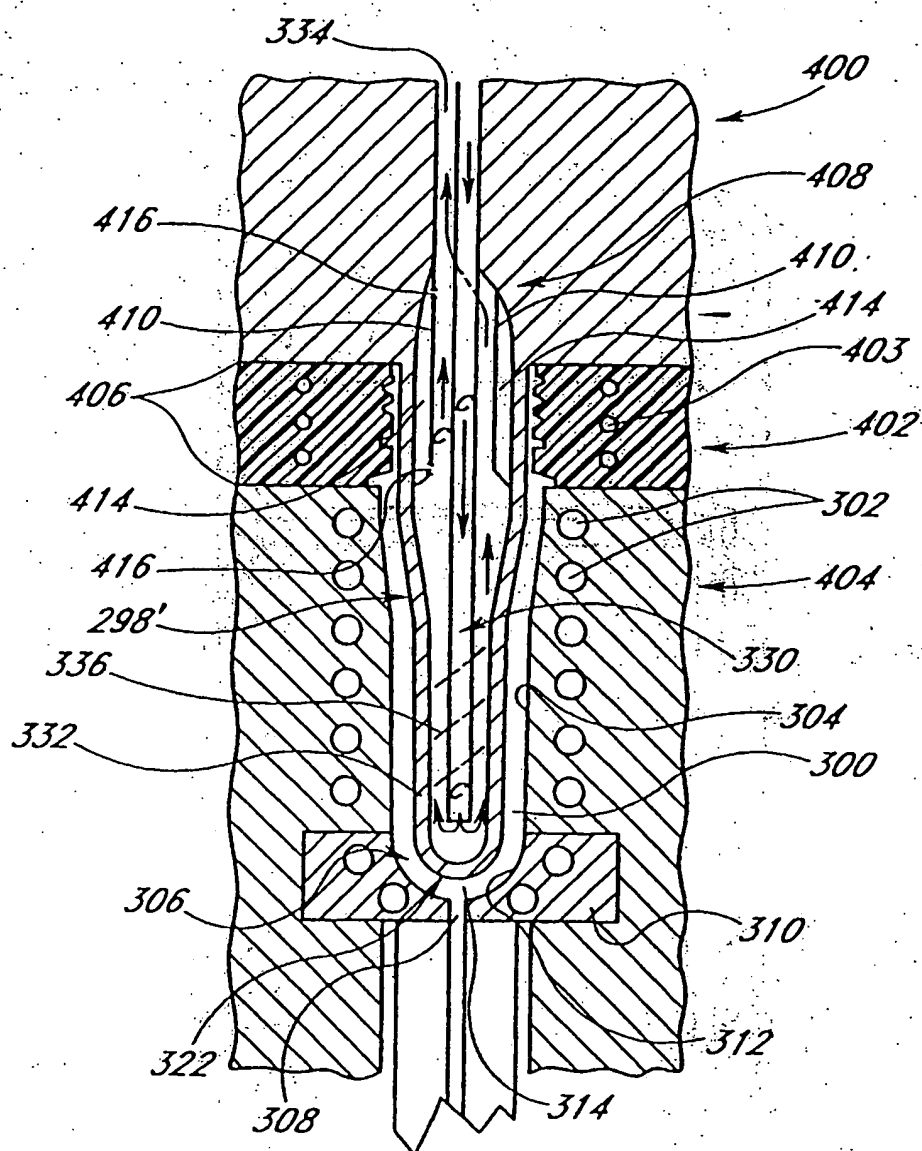
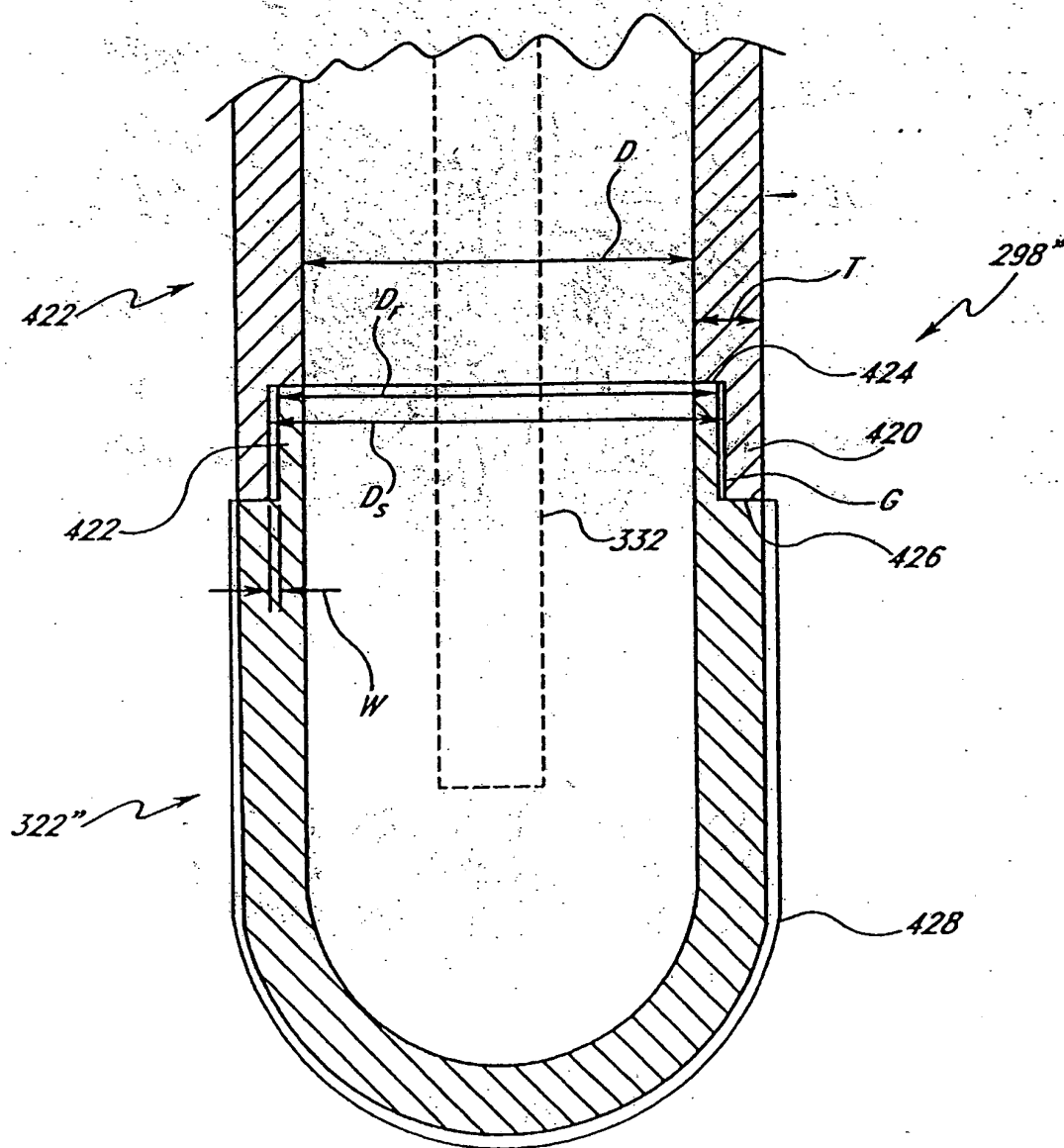


FIG. 18



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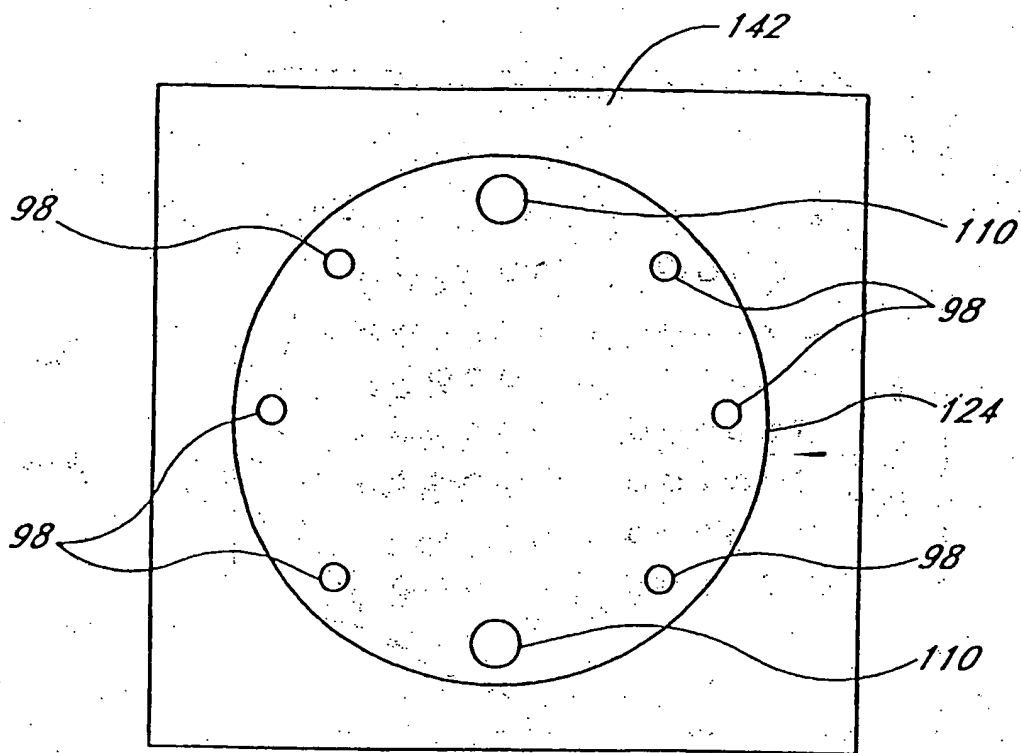


FIG. 8

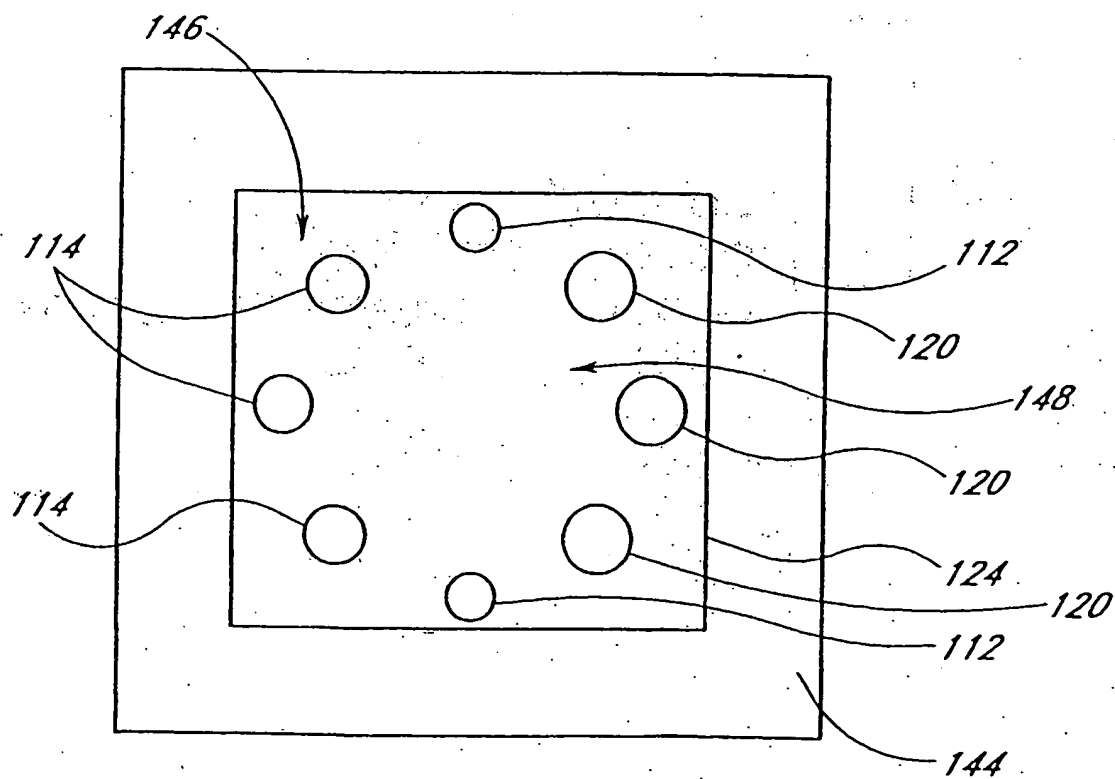


FIG. 9

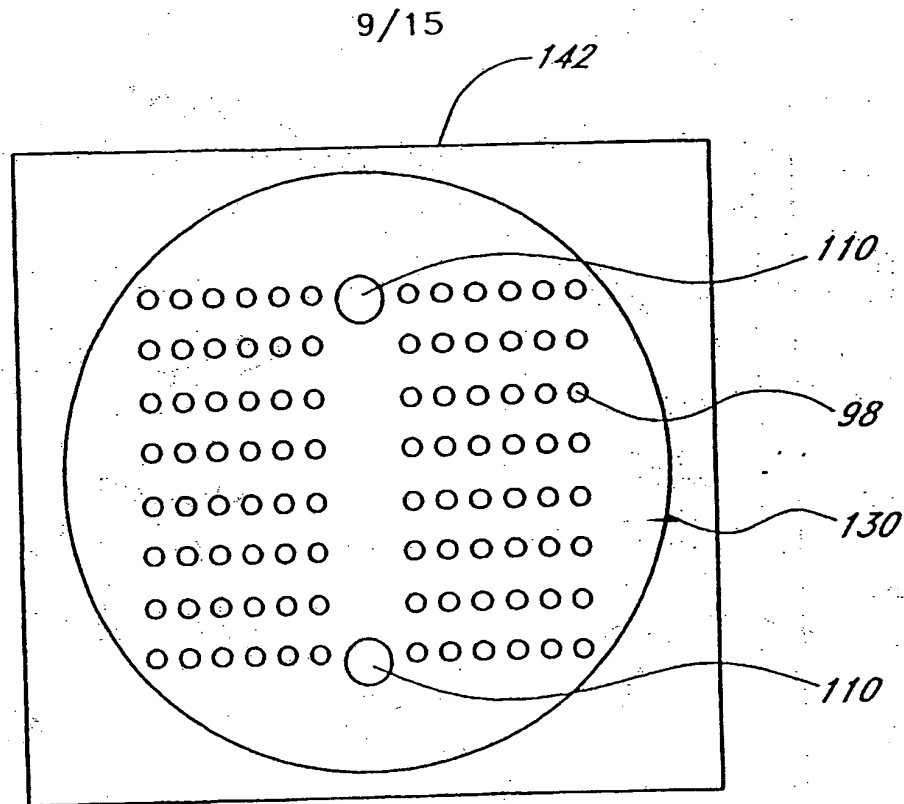


FIG. 10

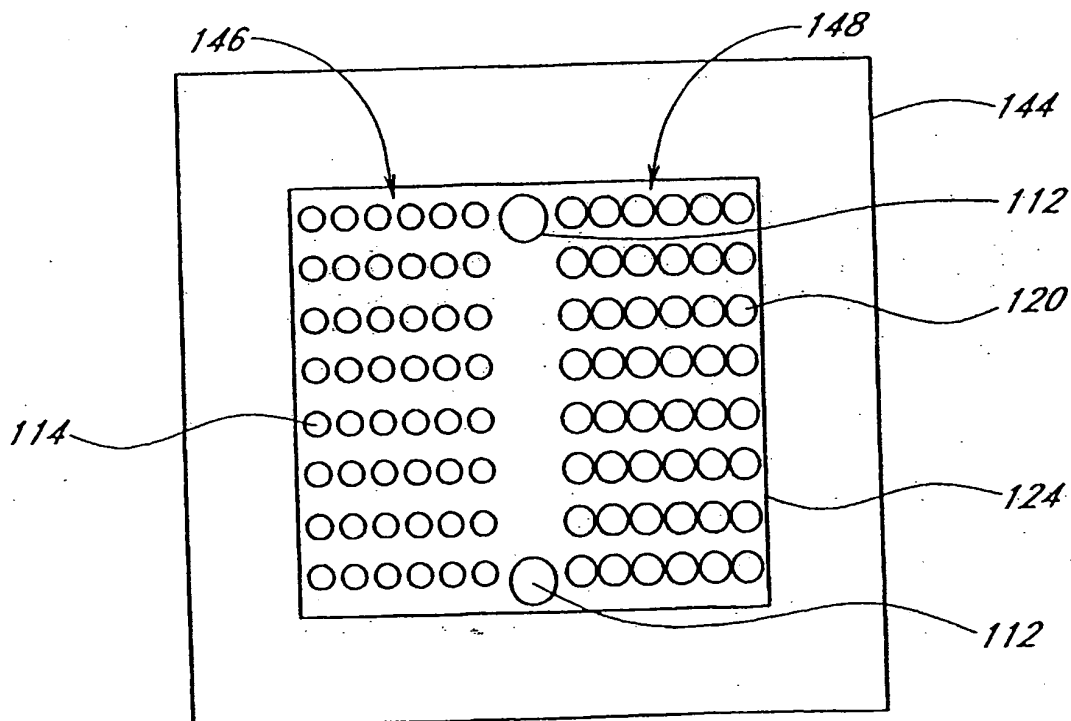
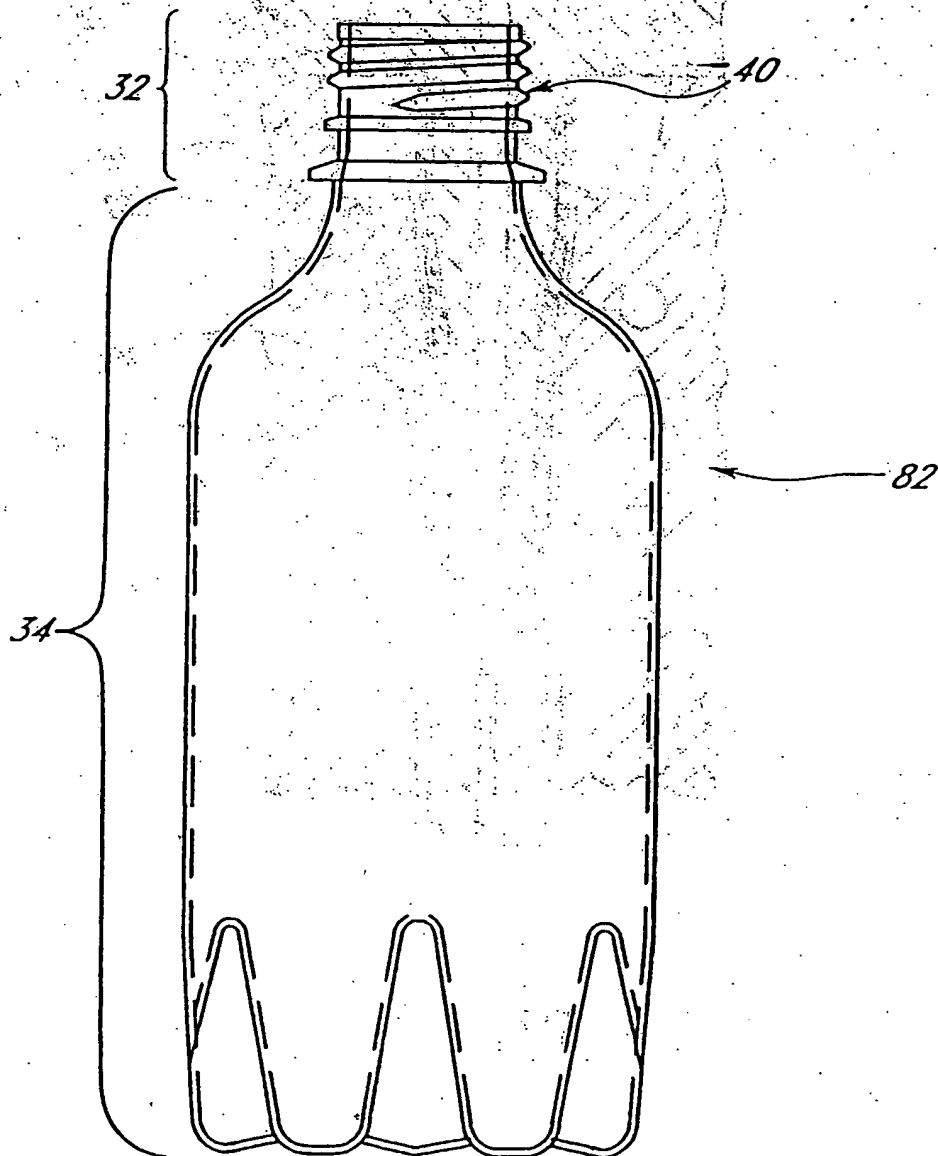


FIG. 11

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**FIG. 6**

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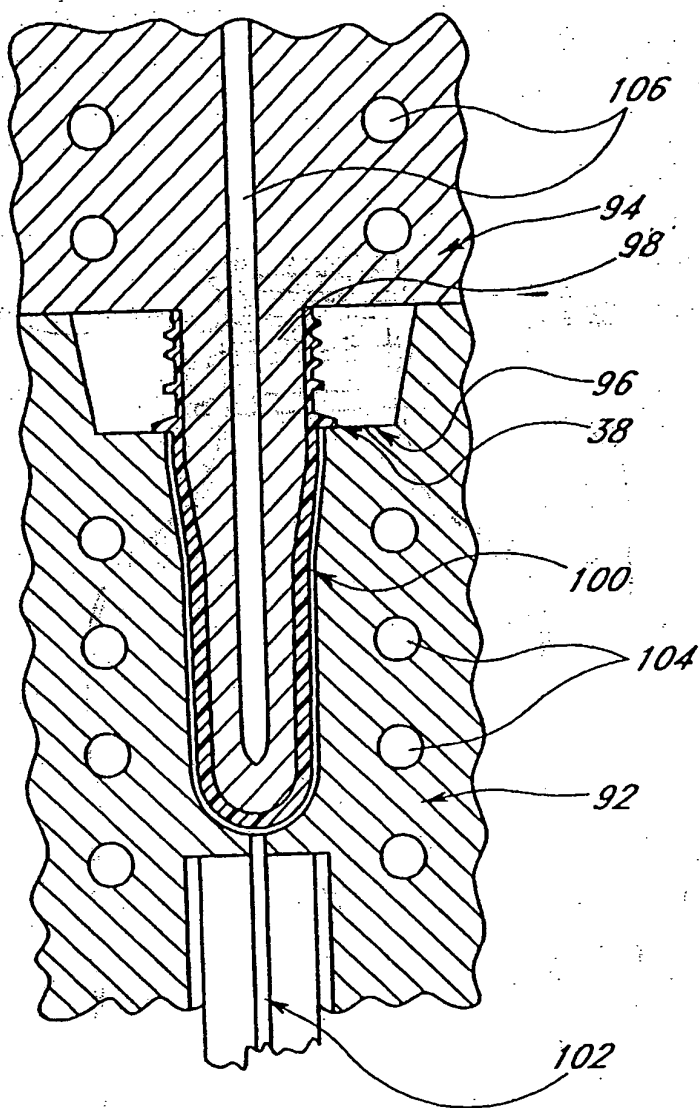


FIG. 7



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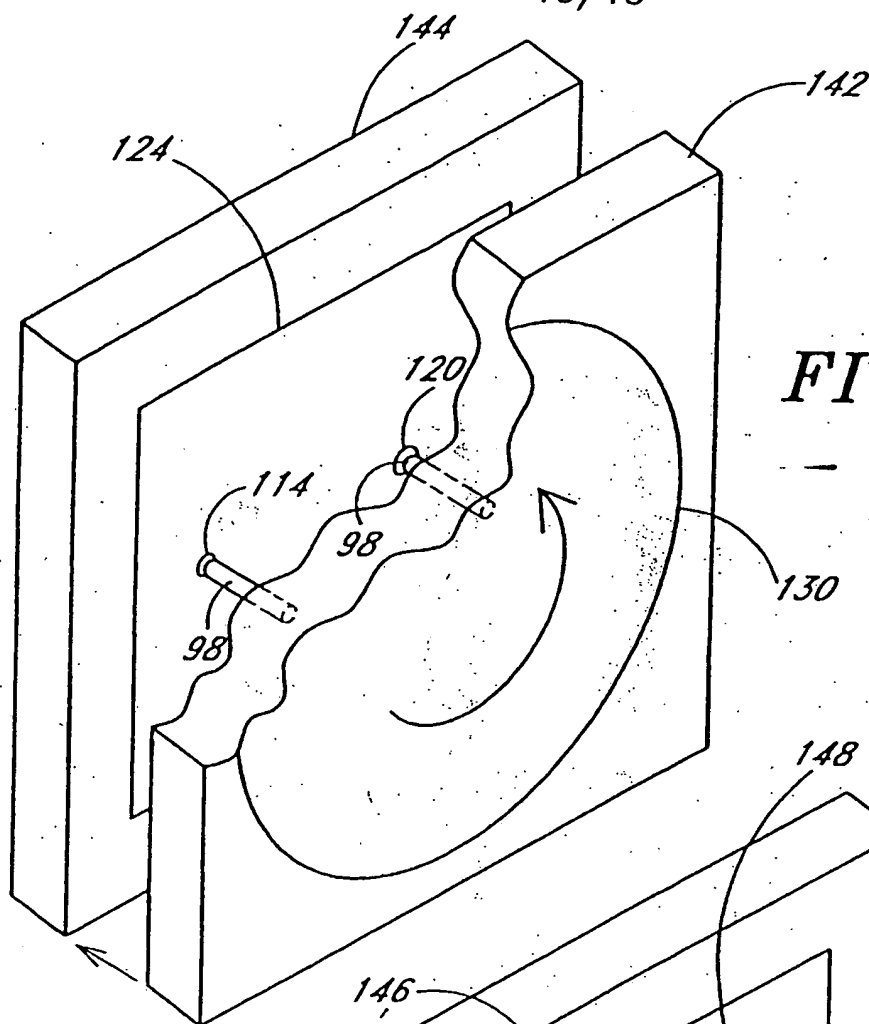
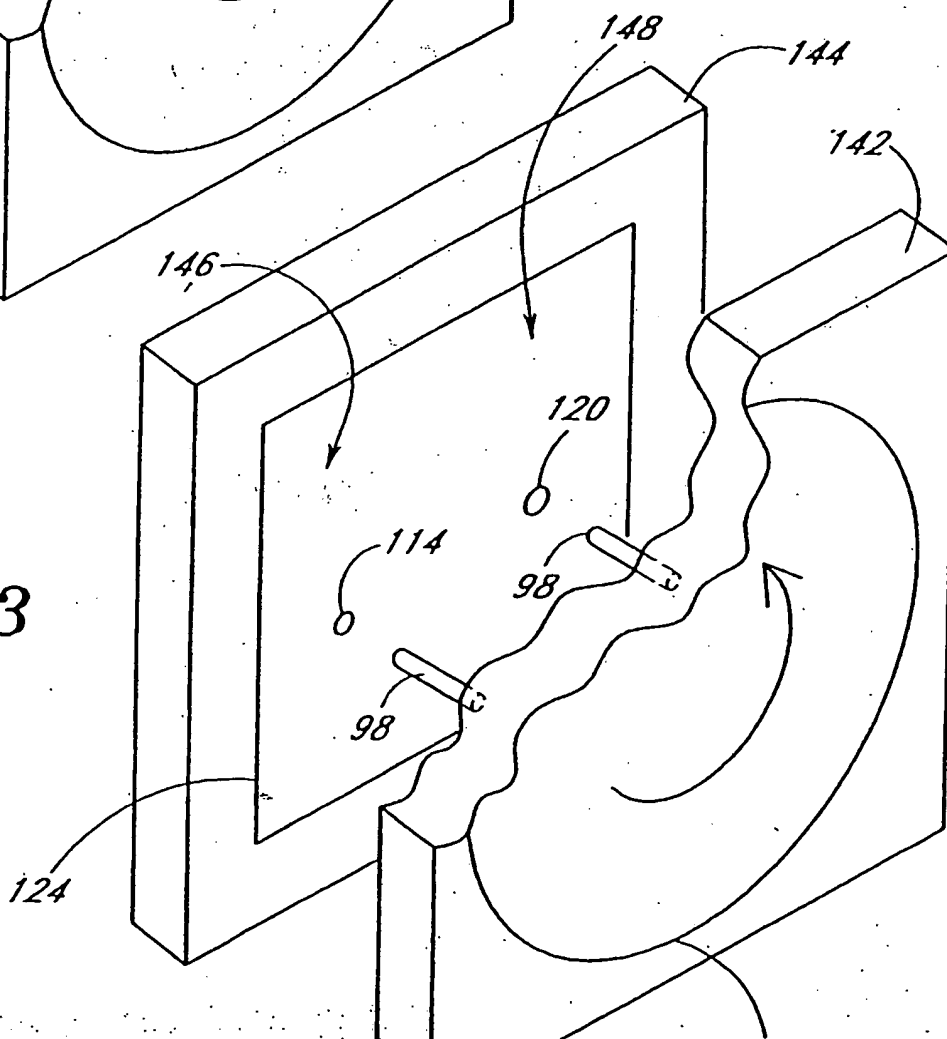


FIG. 12

FIG. 13



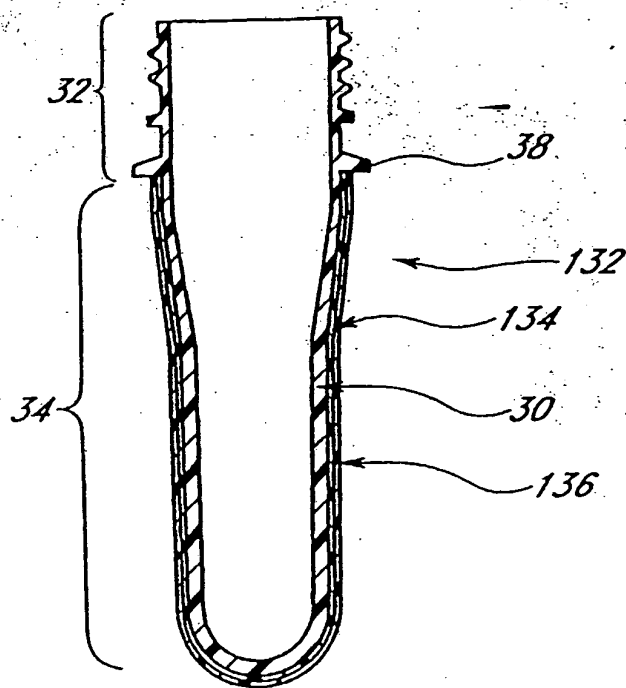


FIG. 14

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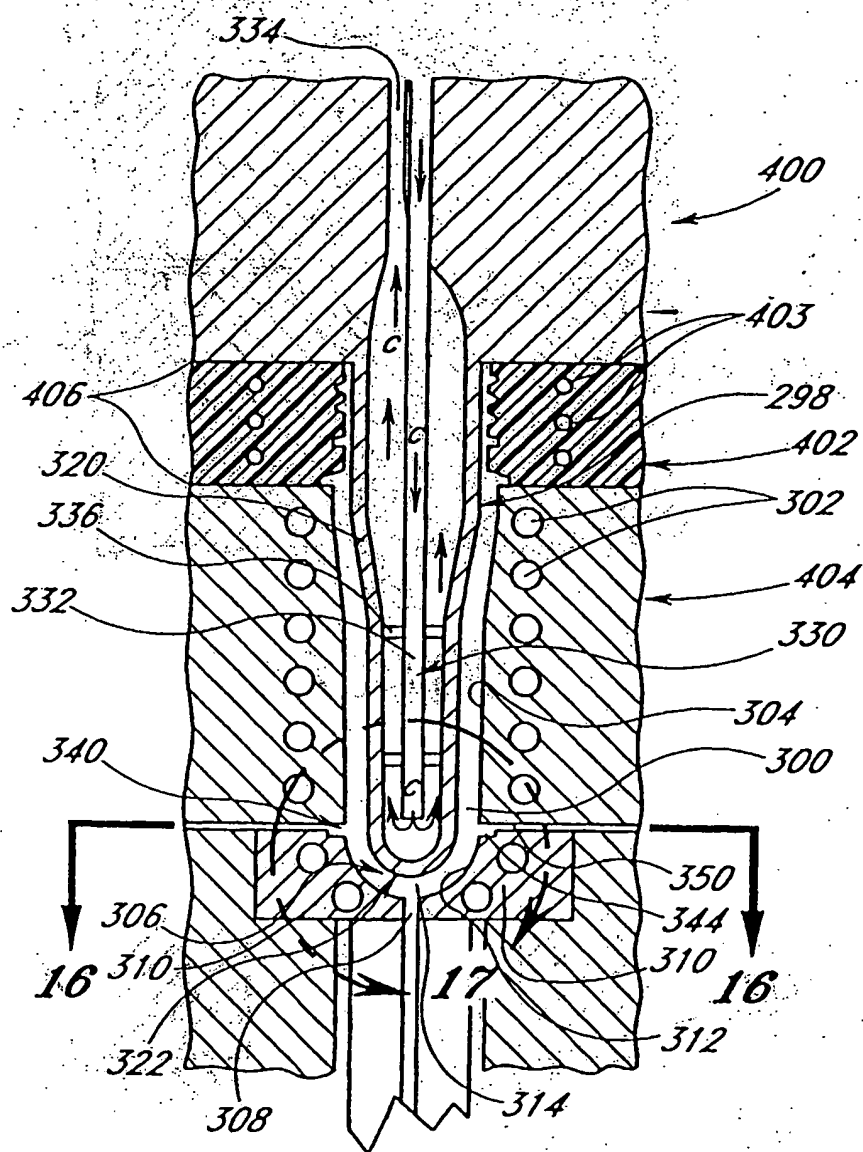


FIG. 15



# INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 01/40618

## A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 B29C45/73 B29C45/14 B29C49/00 B29C49/22

According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 B29C

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

PAJ, WPI Data

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	WO 98 46410 A (HUSKY INJECTION MOLDING) 22 October 1998 (1998-10-22)	1-6, 11-14, 20-22
Y	claims 1-49; figures 1-10	7-10, 15-19
X	PATENT ABSTRACTS OF JAPAN vol. 1999, no. 14, 22 December 1999 (1999-12-22) & JP 11 254510 A (TOPPAN PRINTING CO LTD), 21 September 1999 (1999-09-21) abstract	1-4, 13, 14
X	EP 0 073 151 A (YOSHINO KOGYOSH CO LTD) 2 March 1983 (1983-03-02) claim 1	1-4, 13
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Date of the actual completion of the international search

28 August 2001

Date of mailing of the international search report

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## C. (Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

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X	WO 99 61514 A (EASTMAN CHEM CO) 2 December 1999 (1999-12-02) page 15, line 16 -page 16, line 1	1
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